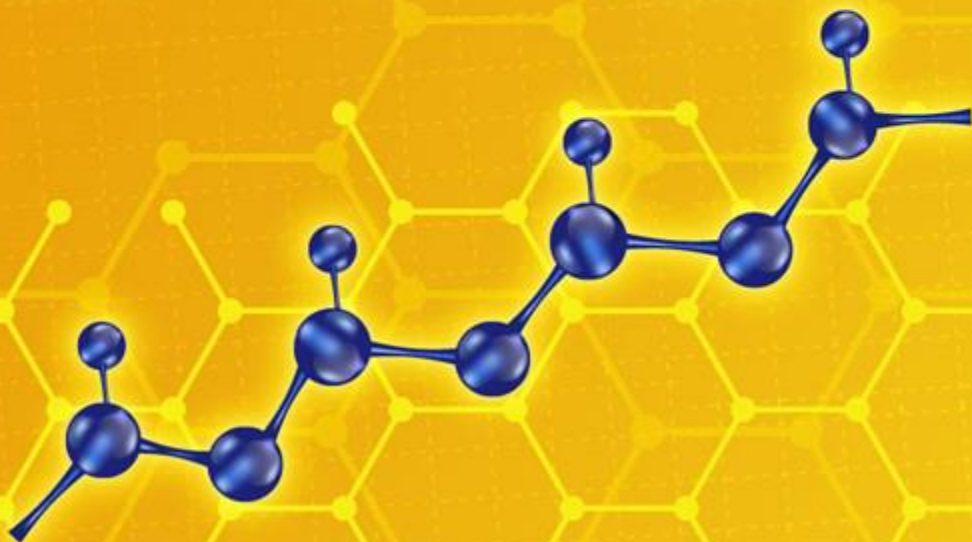




انجمن ملی صنایع پلاستیک ایران

چهارمین همایش ملی

اقتصاد صنایع پلاستیک در ایران ۱۴۰۲



۳۱ خرداد الی آذر ۱۴۰۲



انجمن صنایع پلاستیک ایران

موضوع:

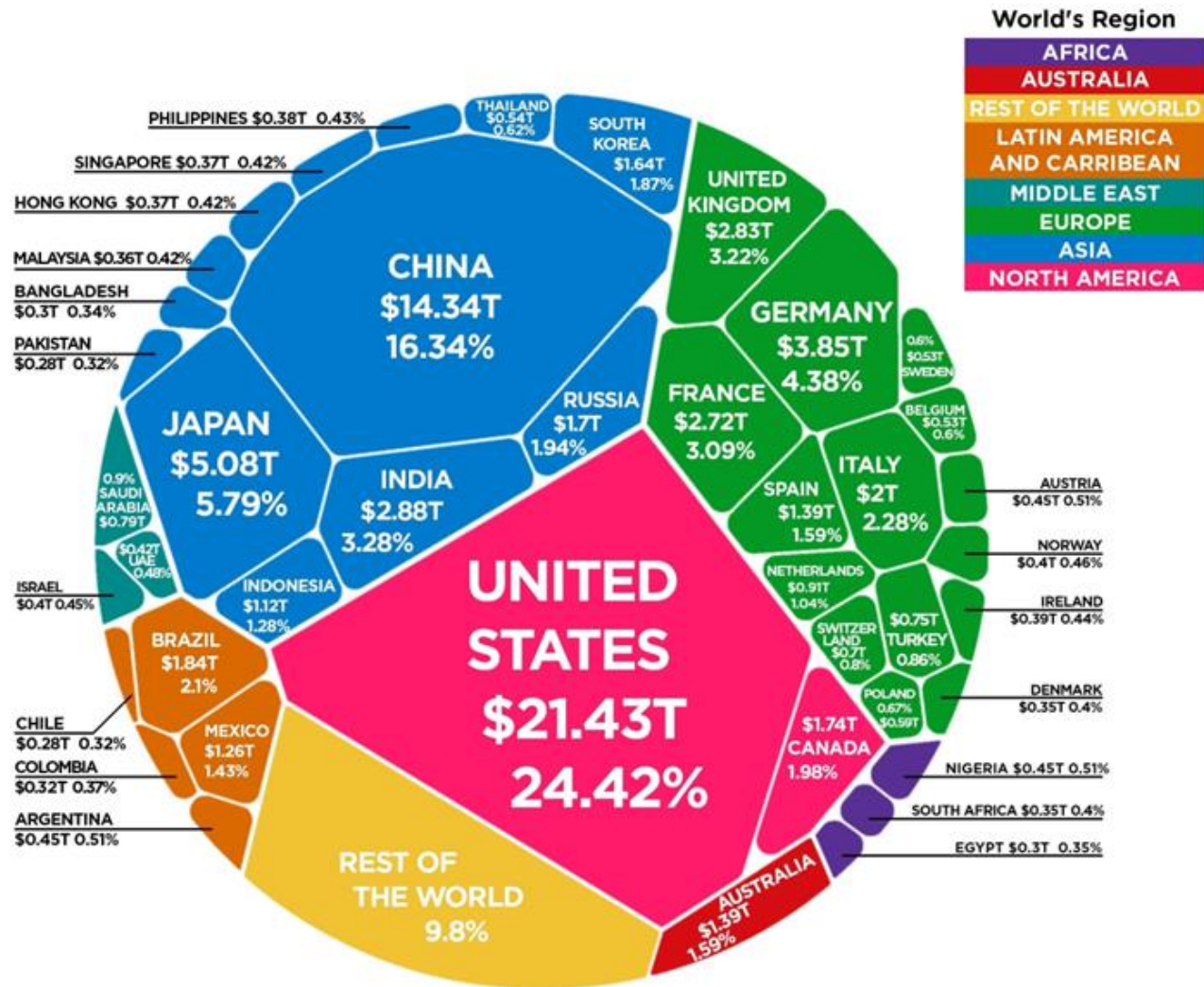
عنوان سخنرانی: بررسی اقتصادی، قوانین روز آمد زیست محیطی و تکنولوژی های نوین بازیافت شیمیایی و مکانیکی پلیمرها

نام سخنران: شروین احمدی





POPULATION	87.920.000
GDP (2021)	531 B USD
Petrochemical products	57 MT/Y



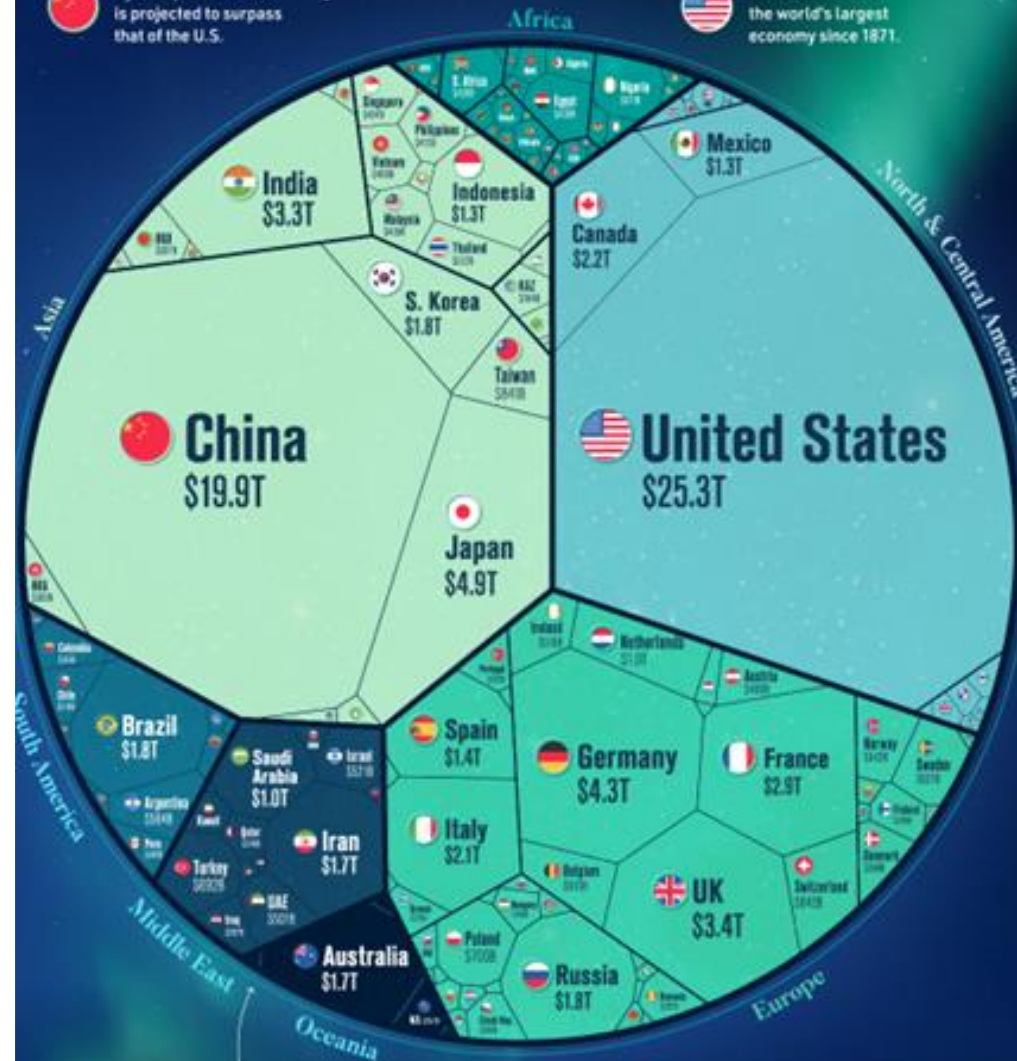
The \$100 Trillion World Economy

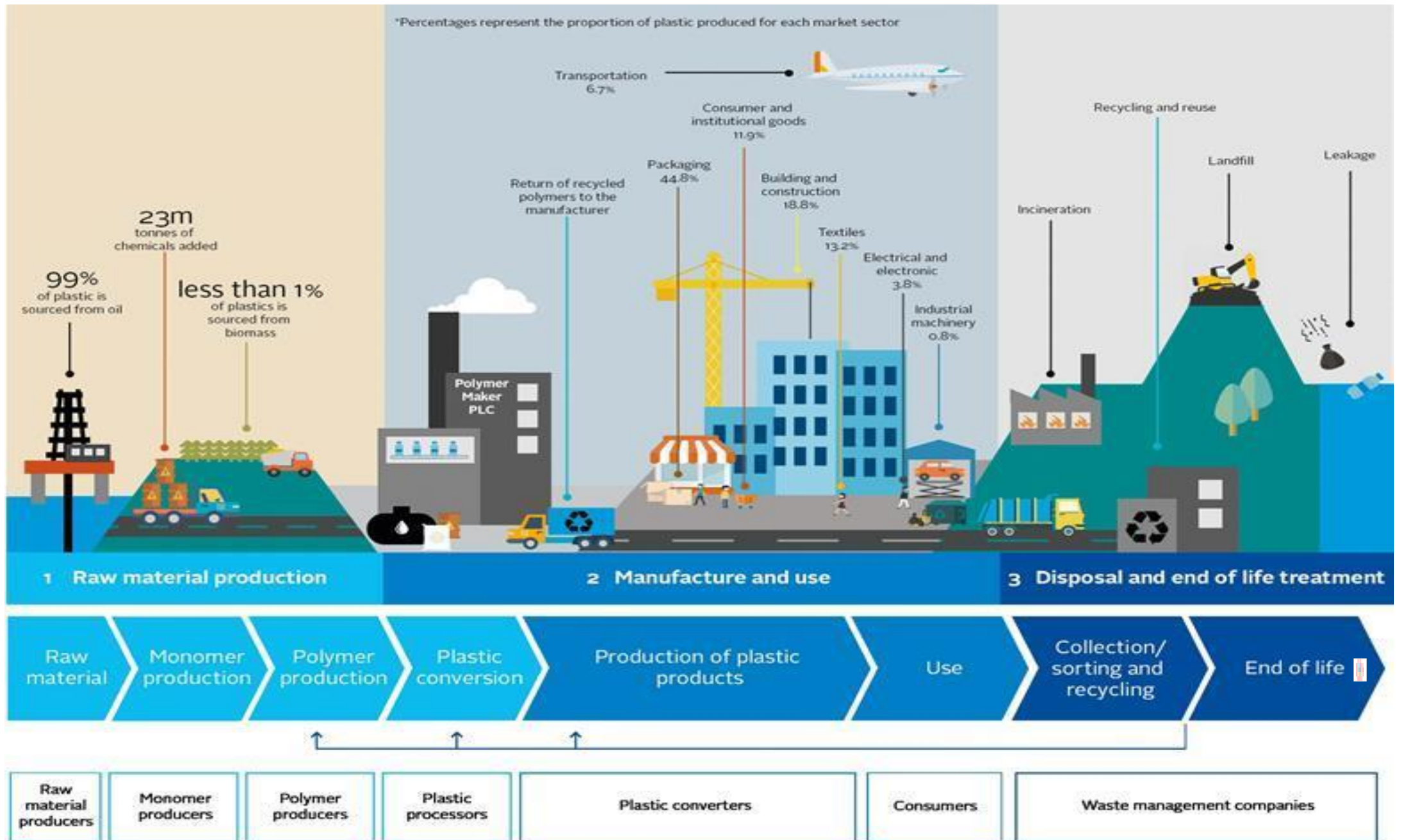
GLOBAL GDP 2022

Despite conflict and looming stagflation, the global economy will hit an impressive new milestone, reaching **\$104 trillion**, according to the latest IMF projections for end of year.

By 2030, China's GDP is projected to surpass that of the U.S.

The U.S. has been the world's largest economy since 1871.



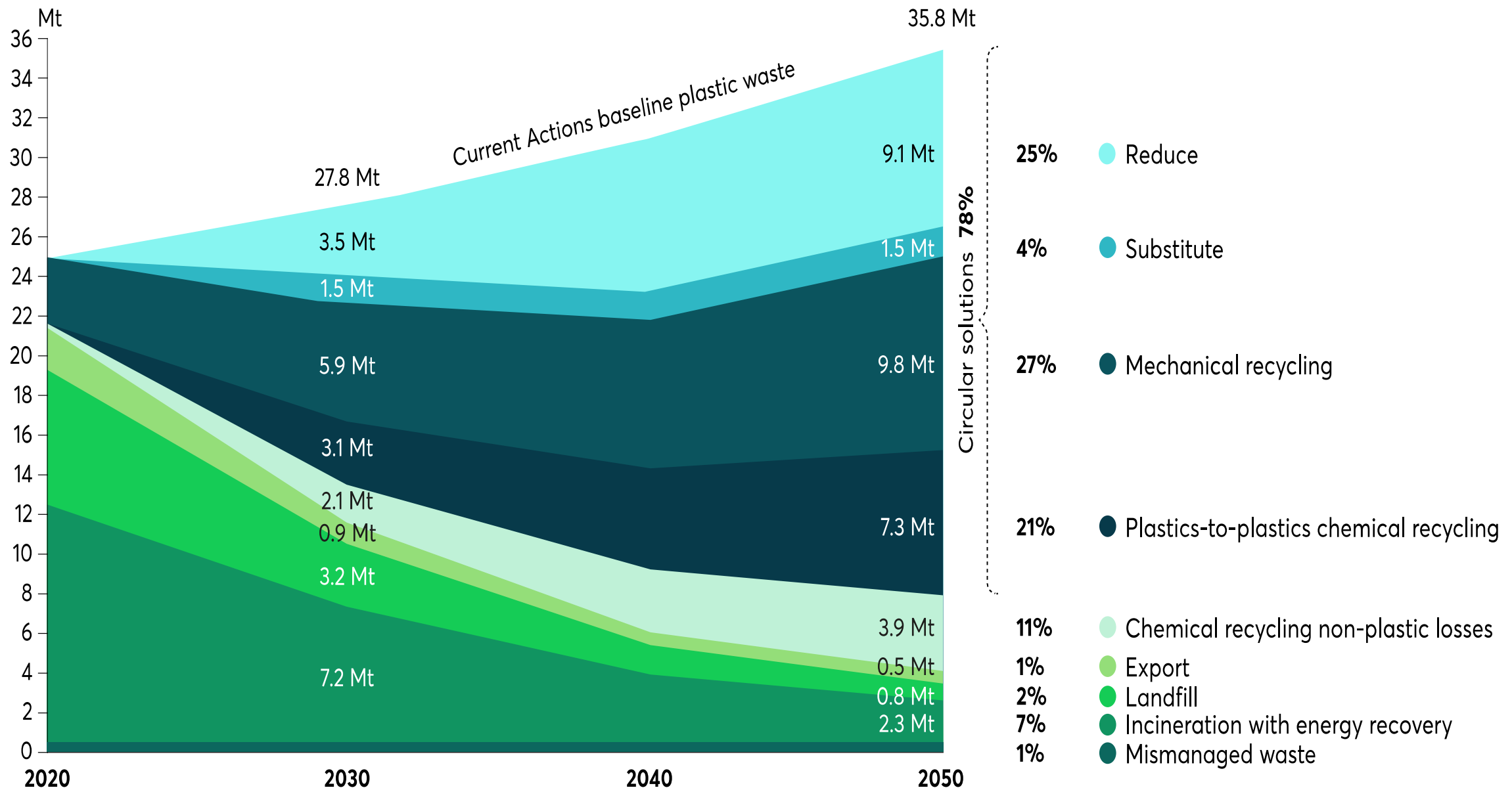


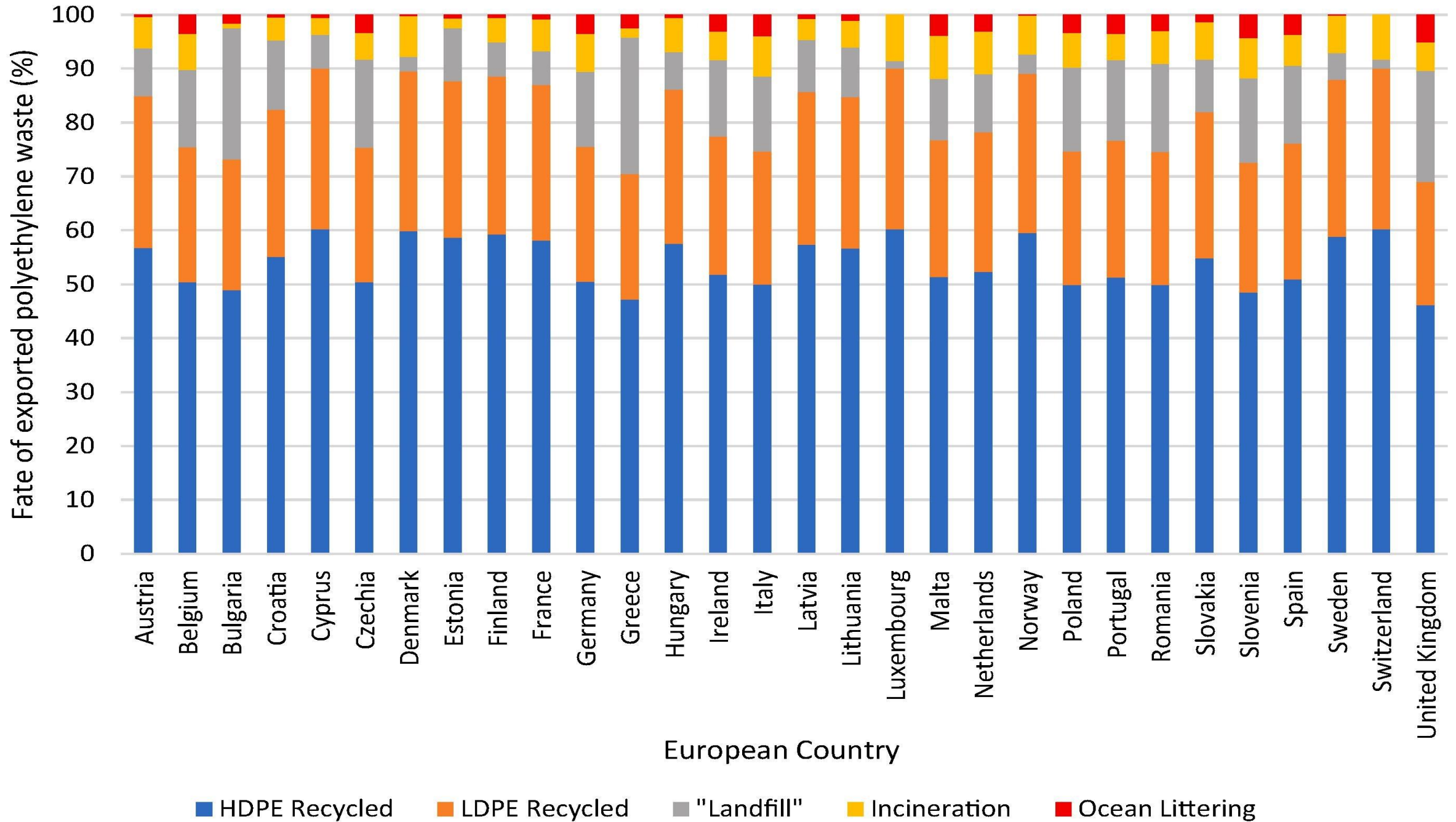


Sustainability



Circular strategies, technologies, and transition companies are looking beyond traditional economic models.





Plastics waste rules and regulations

HS code 3915

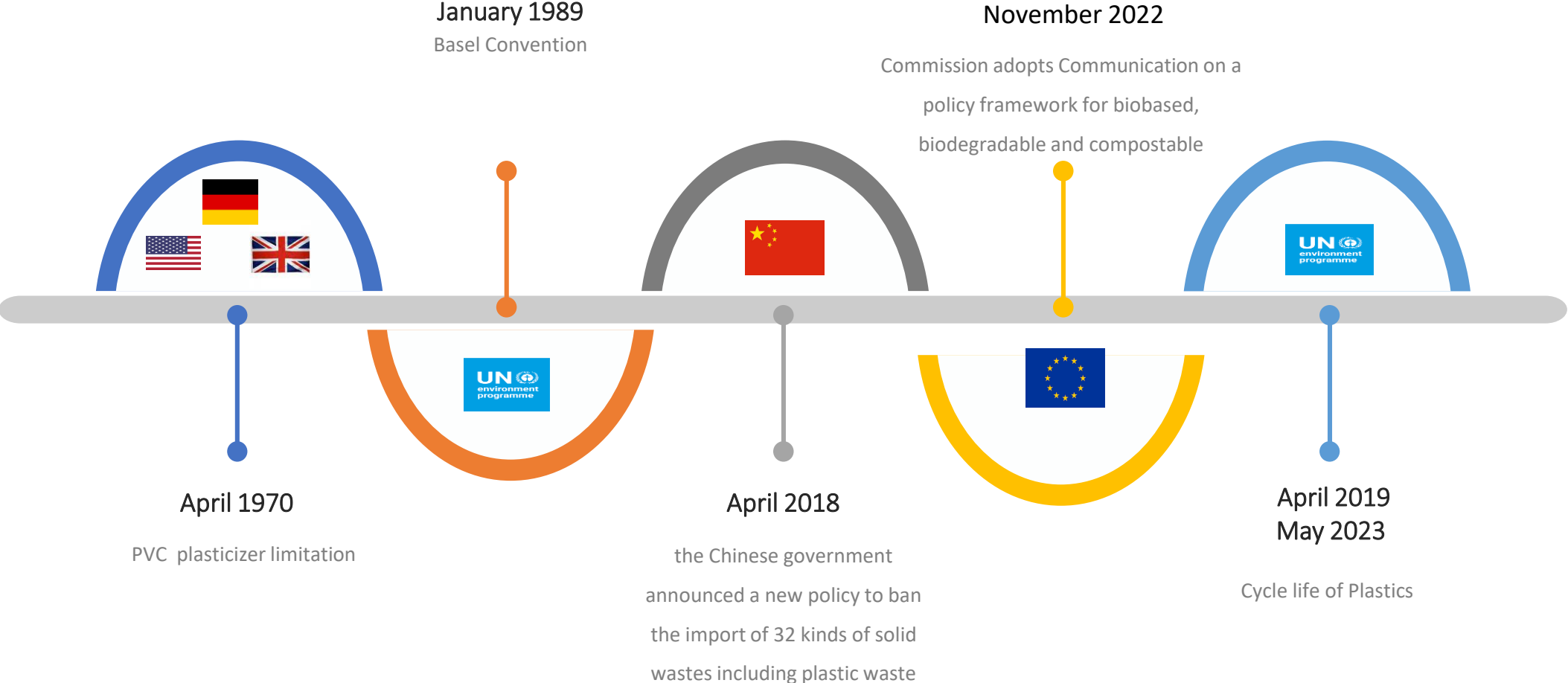
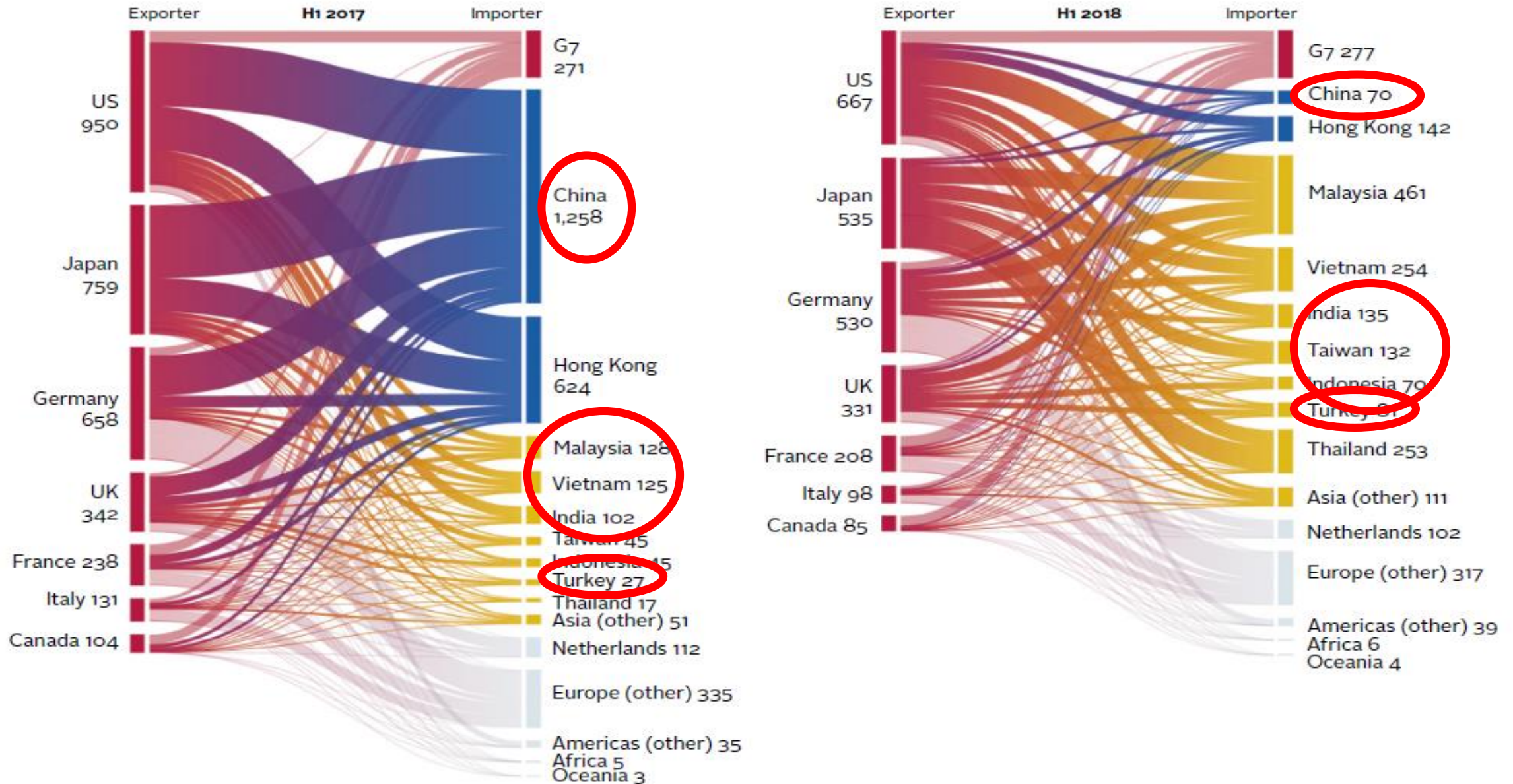
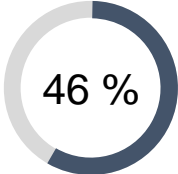


Figure : Global flows of plastic waste and the impact of China's restrictions on plastic imports in 2018. Source: FT

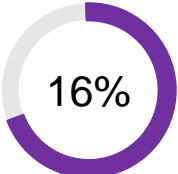
Exports of plastic waste, parings and scrap from G7 countries ('000 tonnes)



PLASTIC WASTE MARKET, BY REGION 2024 – 37.9USD B



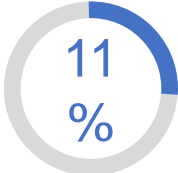
ASIA



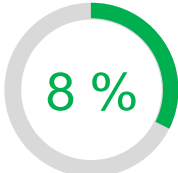
N-AMERICA



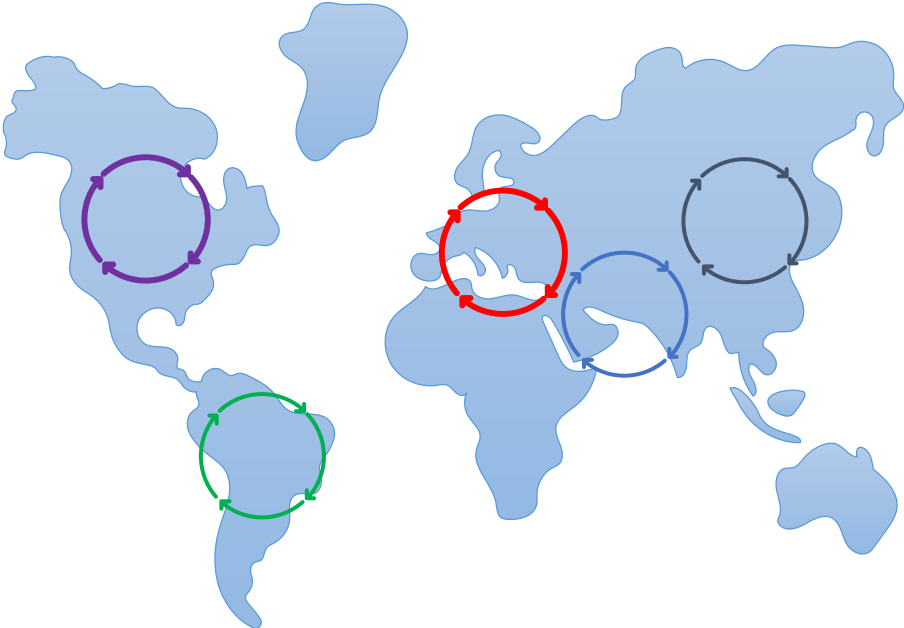
EUROP



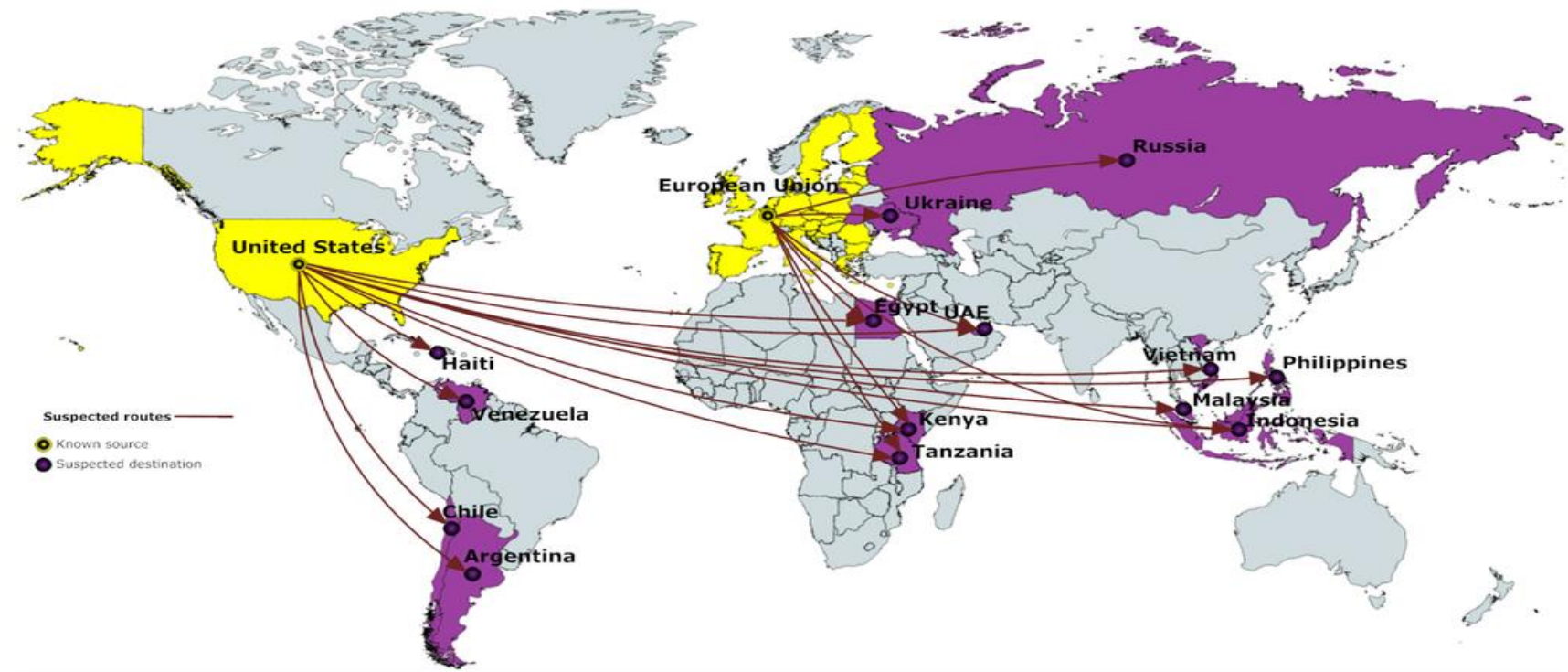
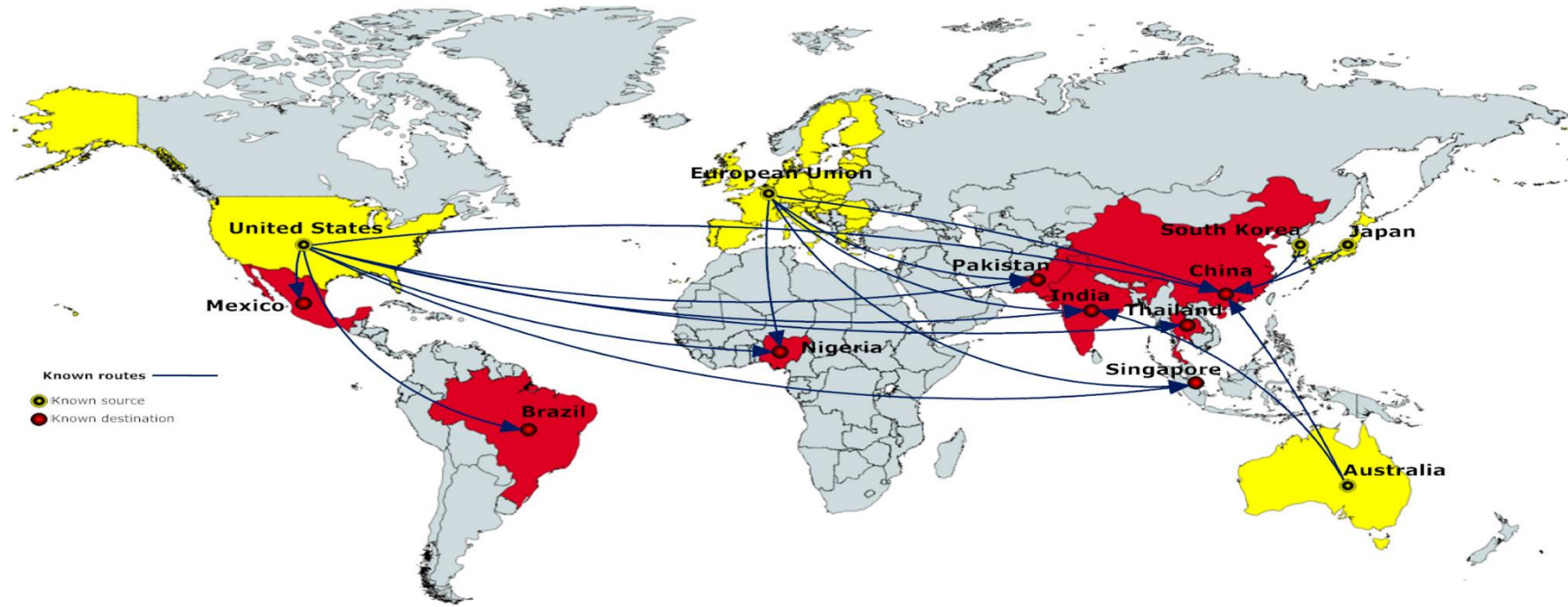
Middle E &
AFRICA



S- AMERICA



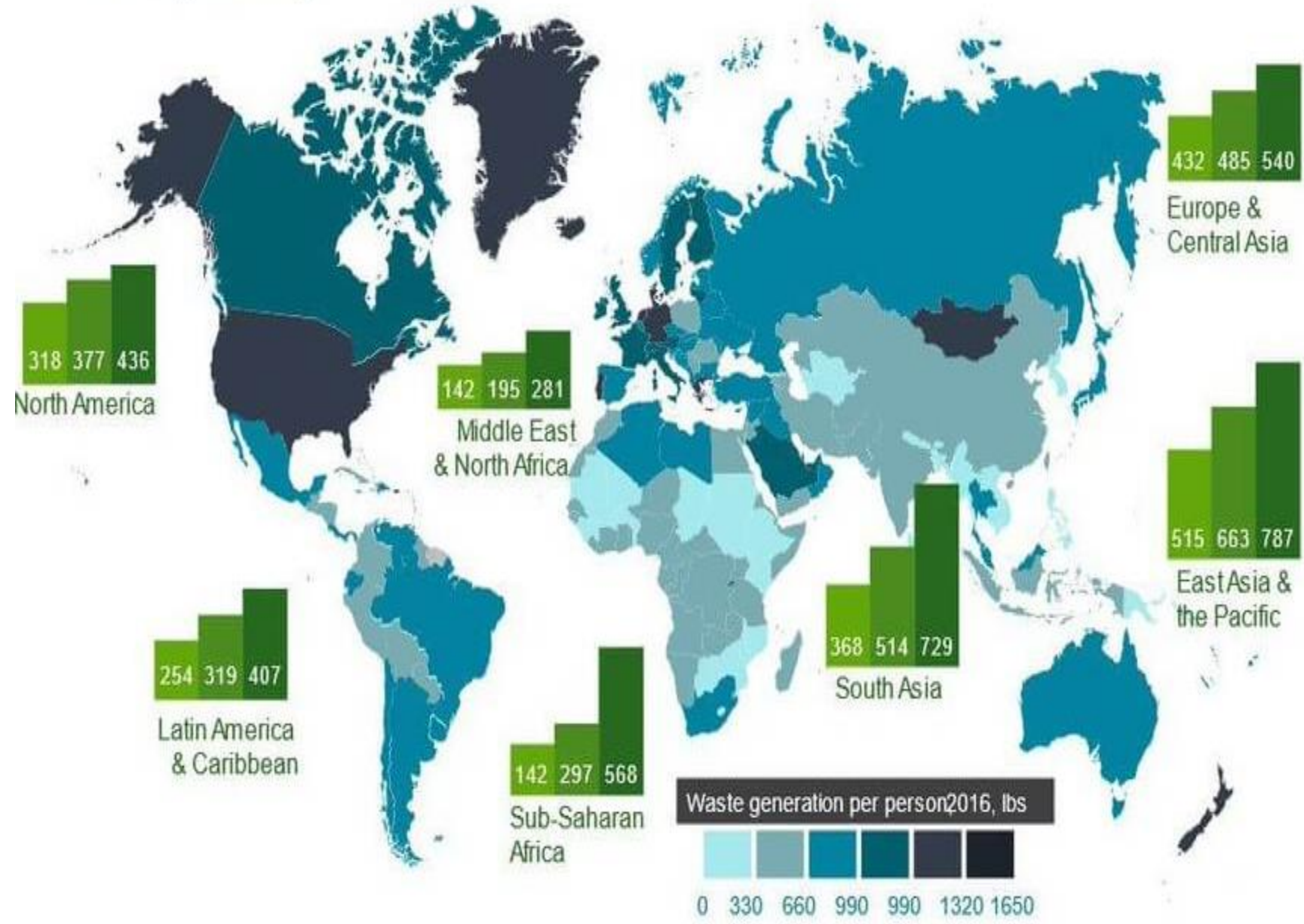
Known routes of illegal e-waste trade



• **A THROWAWAY WORLD**

Regional waste generation
US ton (millions)

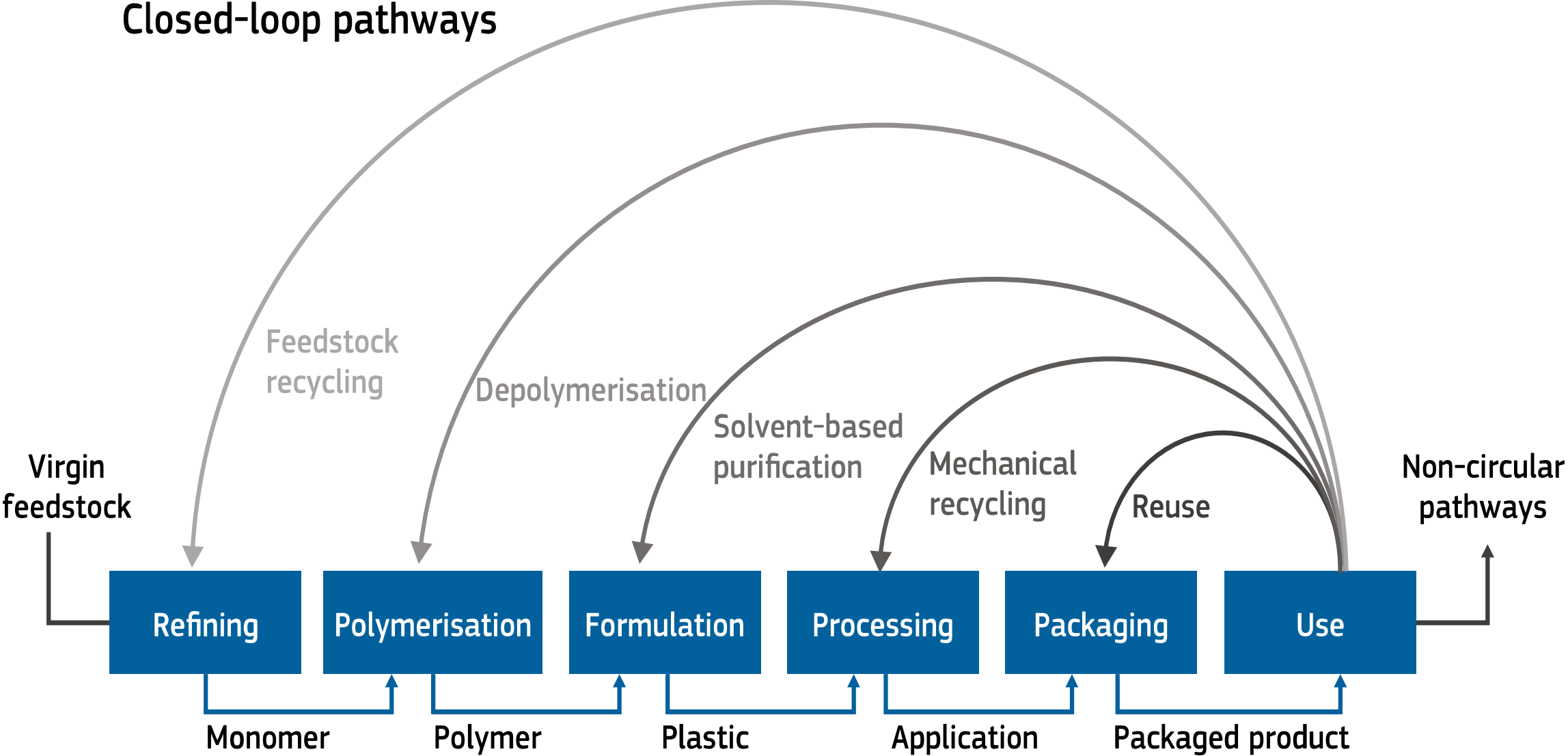
2016 2030 forecast 2050 forecast

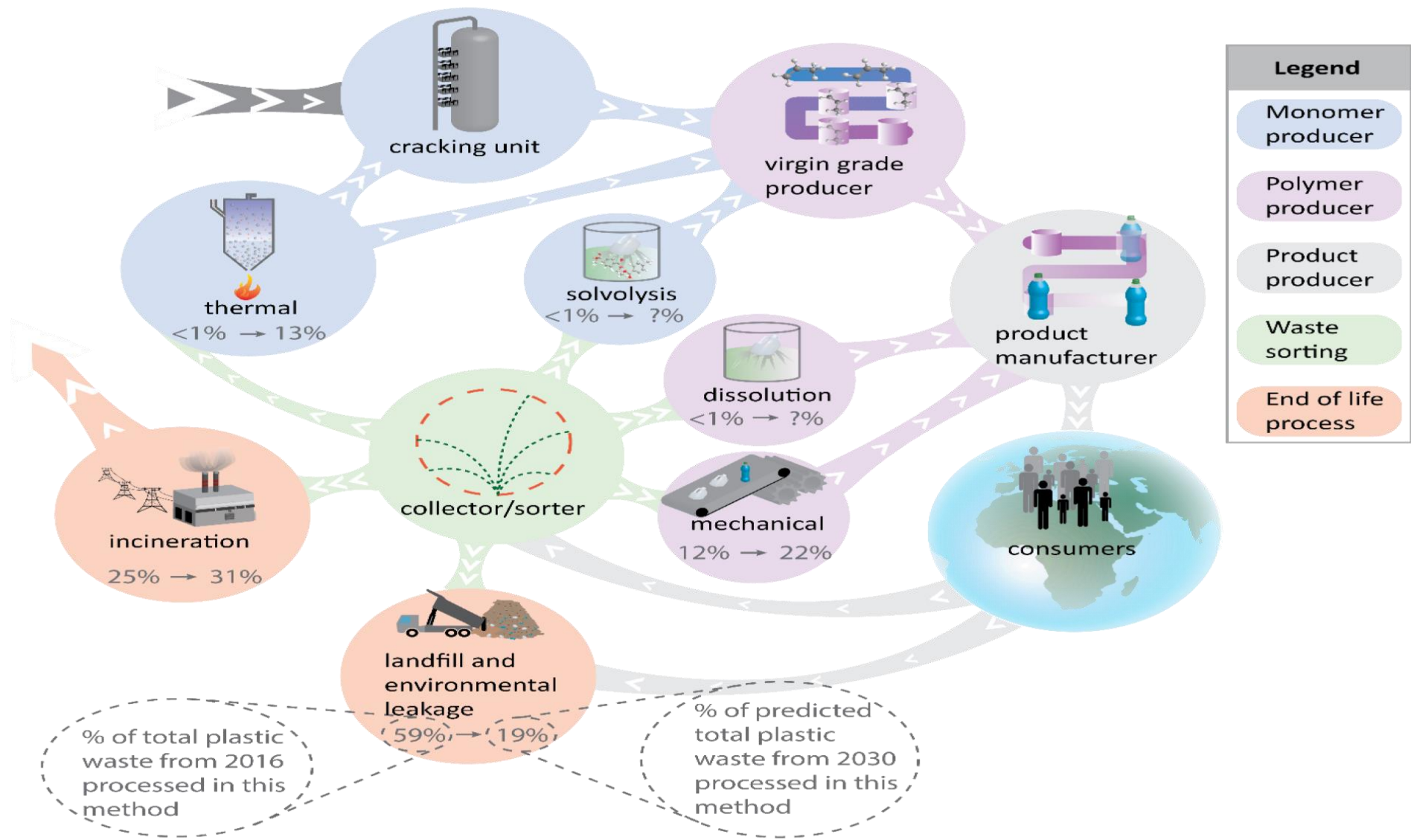


Recycling

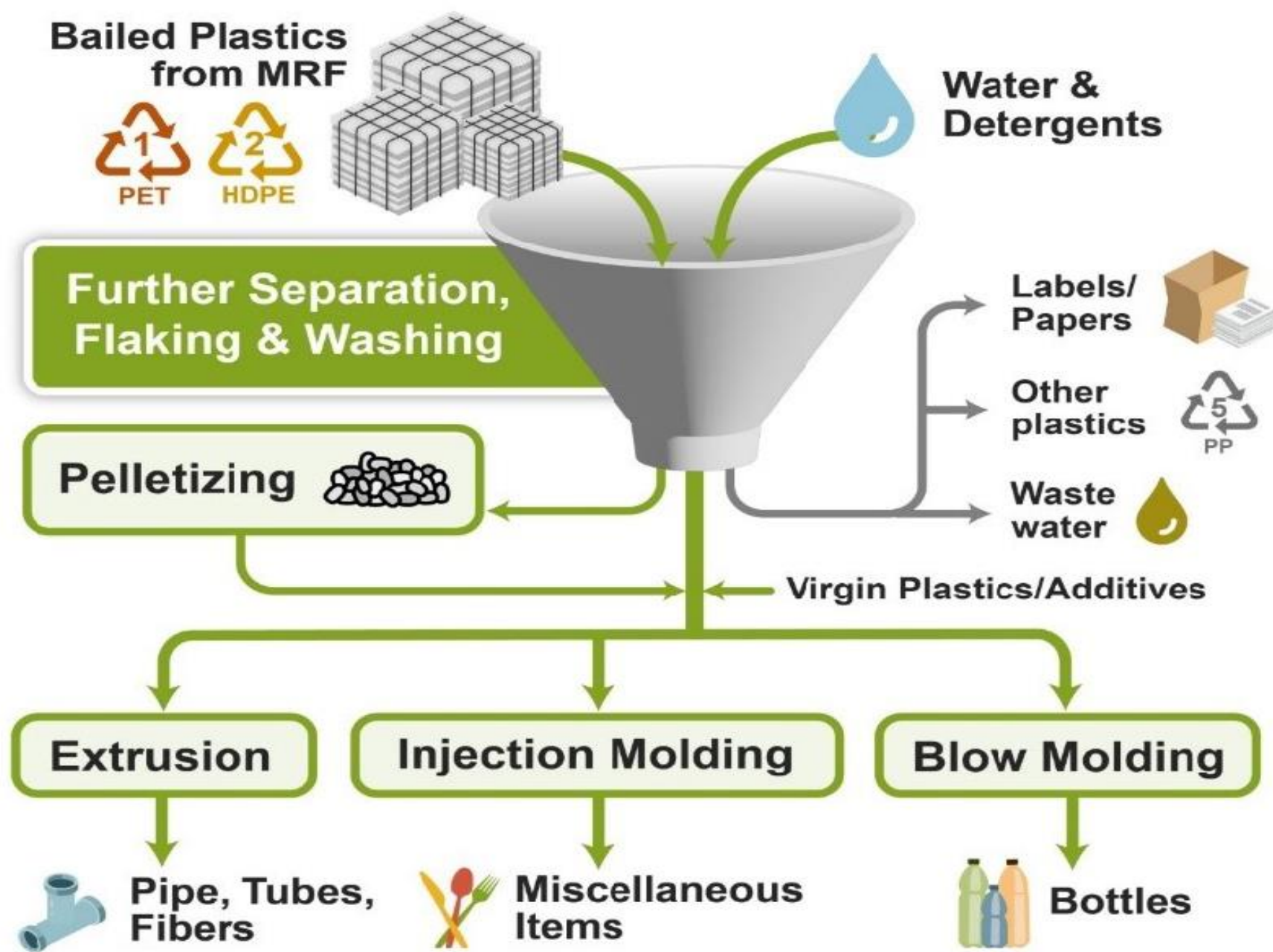


Closed-loop pathways

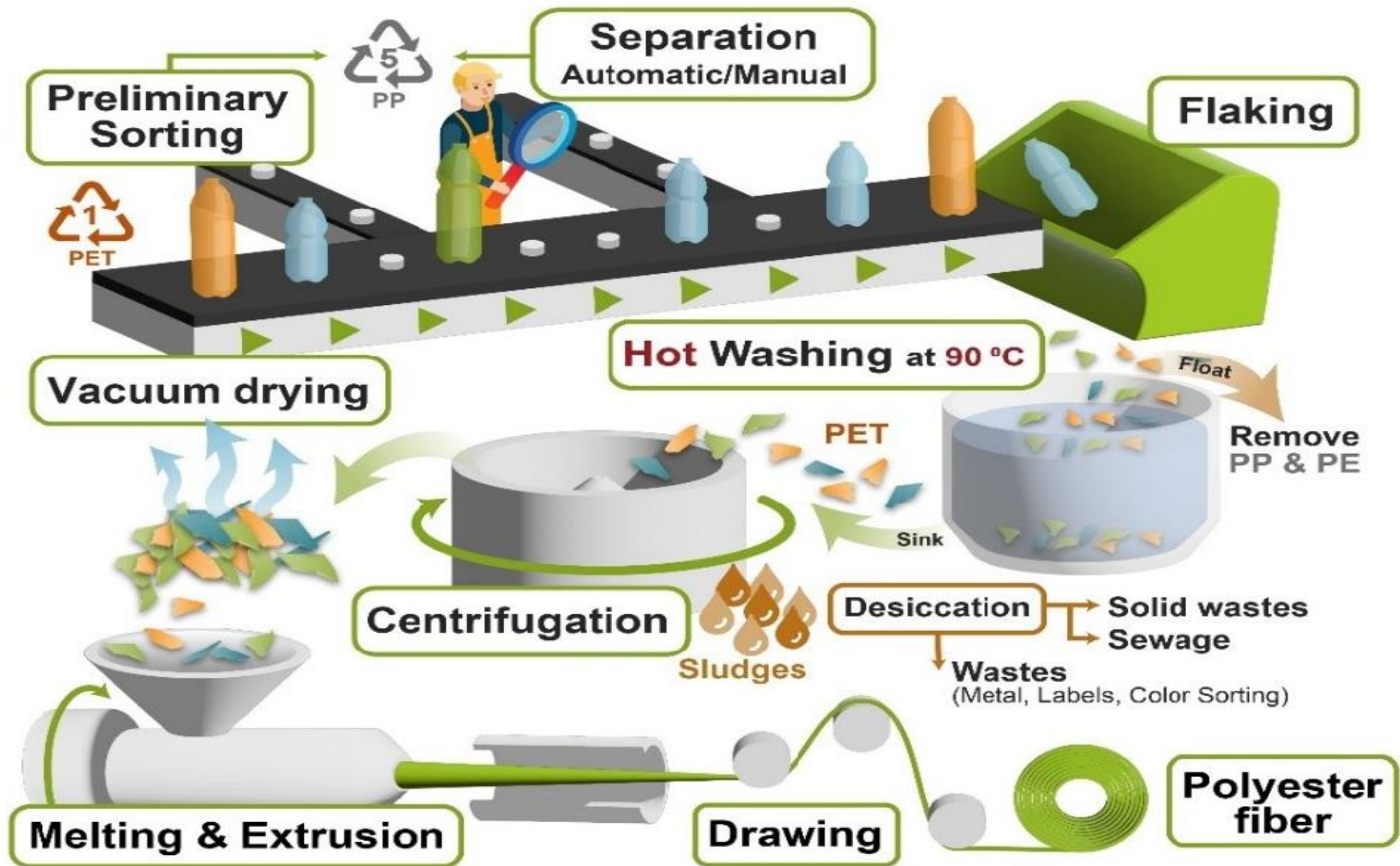




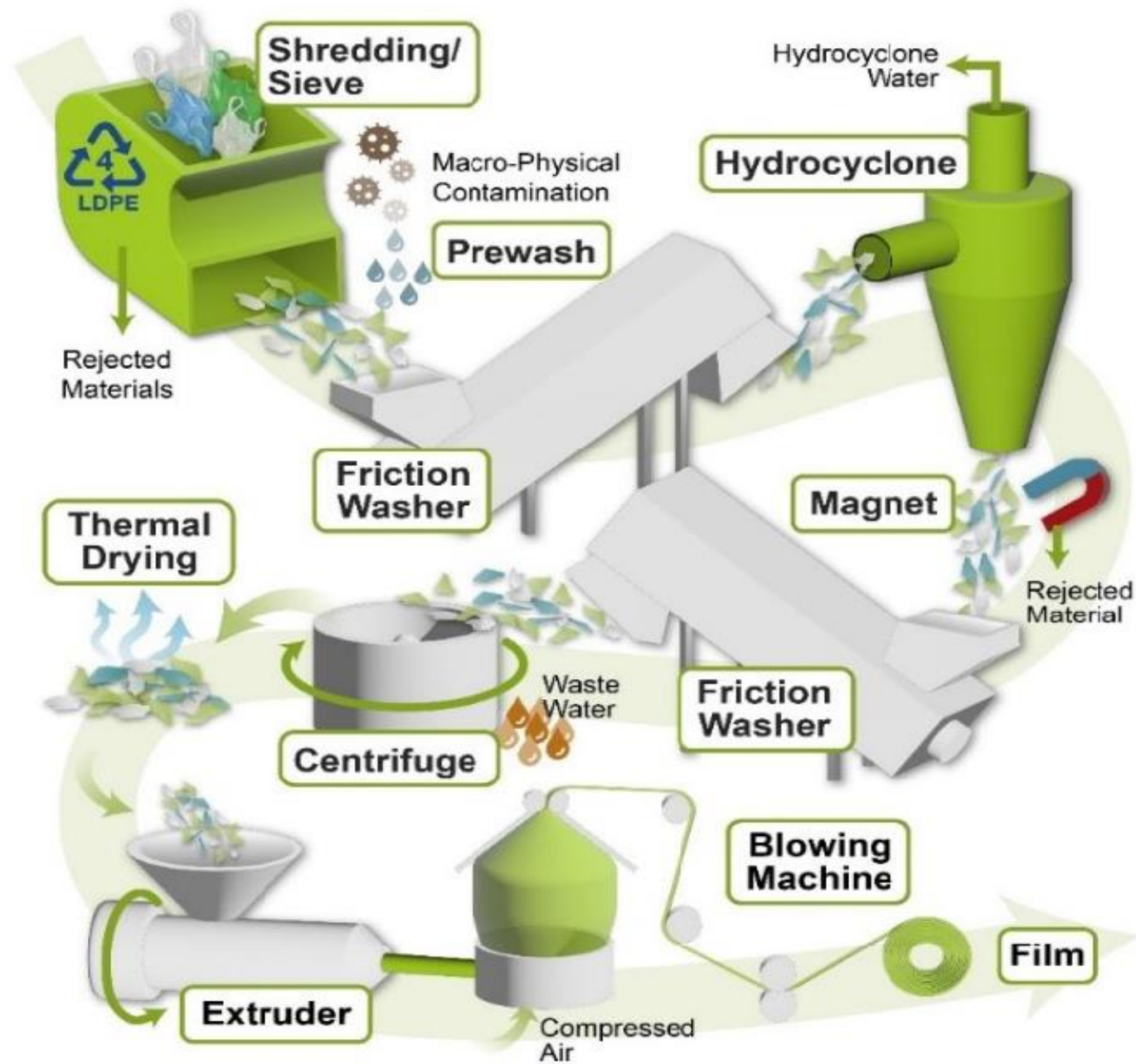
Mechanical Recycling



Various approaches for mechanical recycling of PSW (Plastic solid waste).

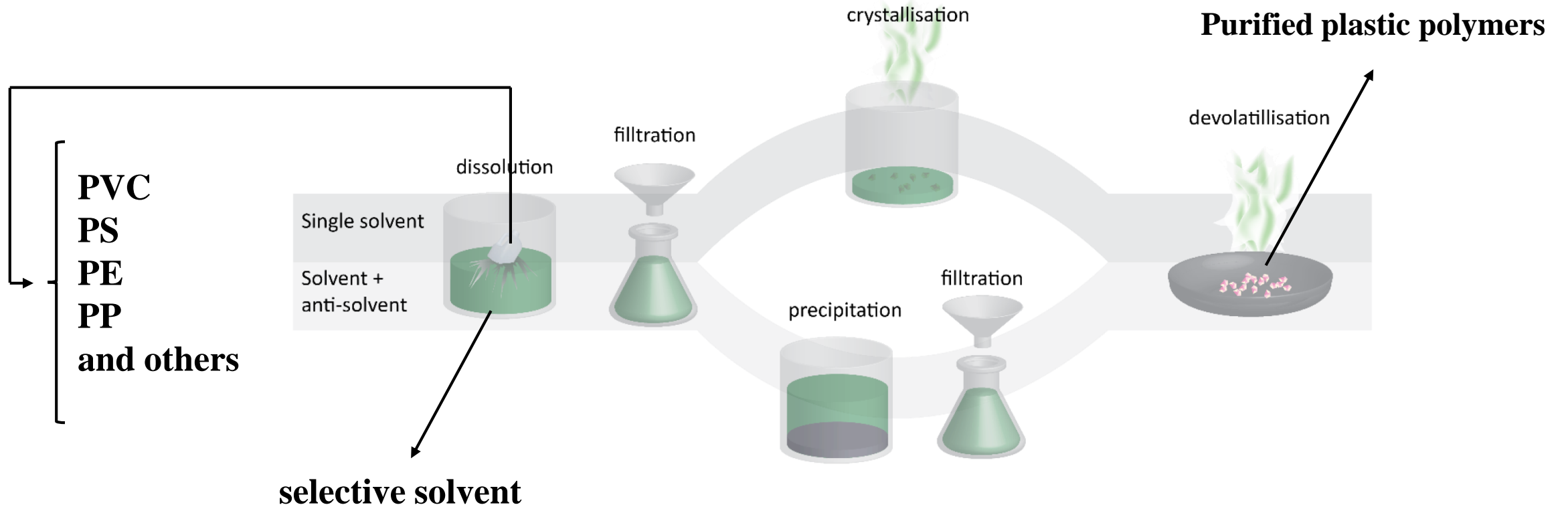


A generalized process flow diagram for a recycling of PET bottles.

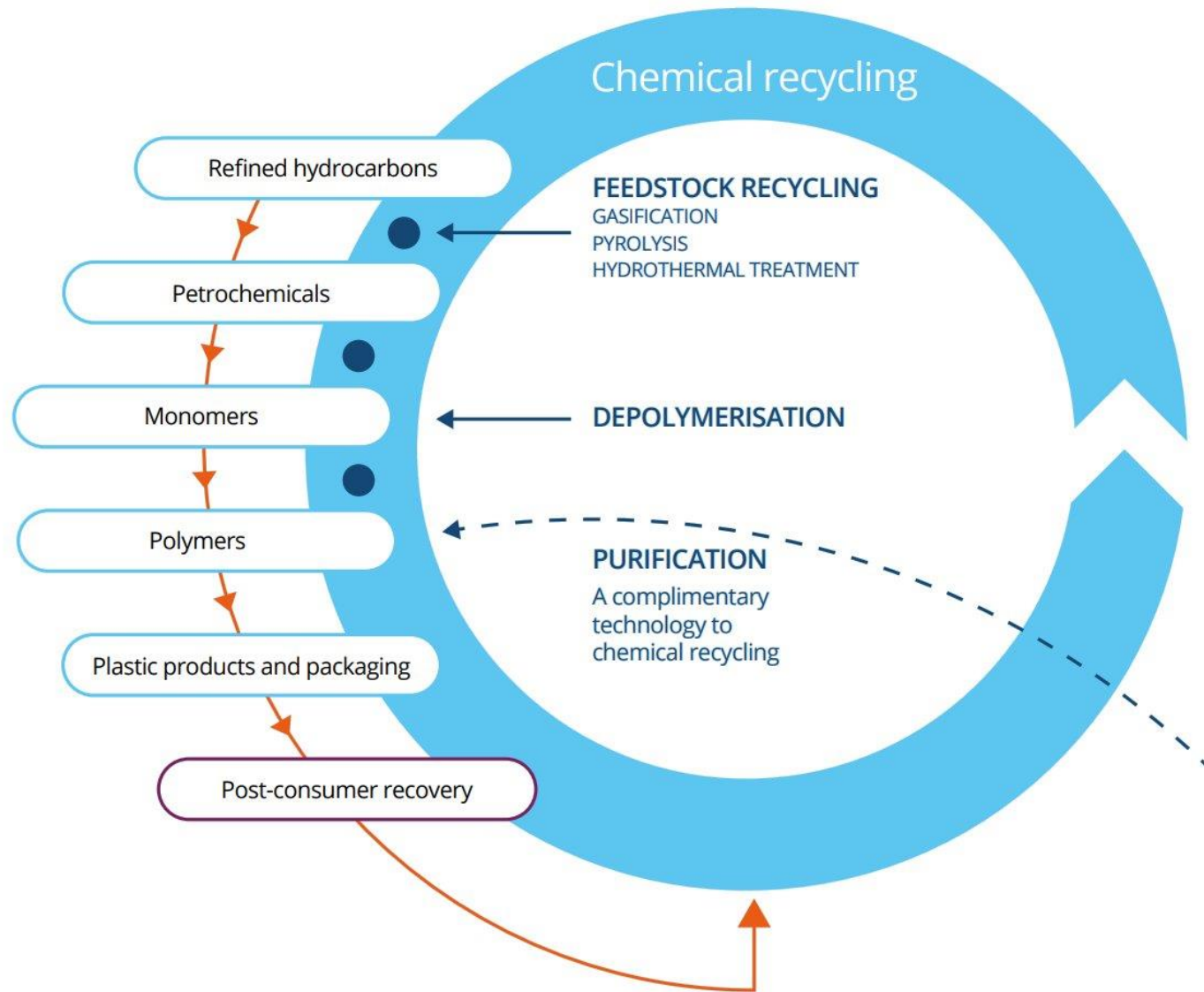


Mechanical recycling process of polyethylene plastic film at an industrial plant.

Purification (Dissolution/precipitation processes)

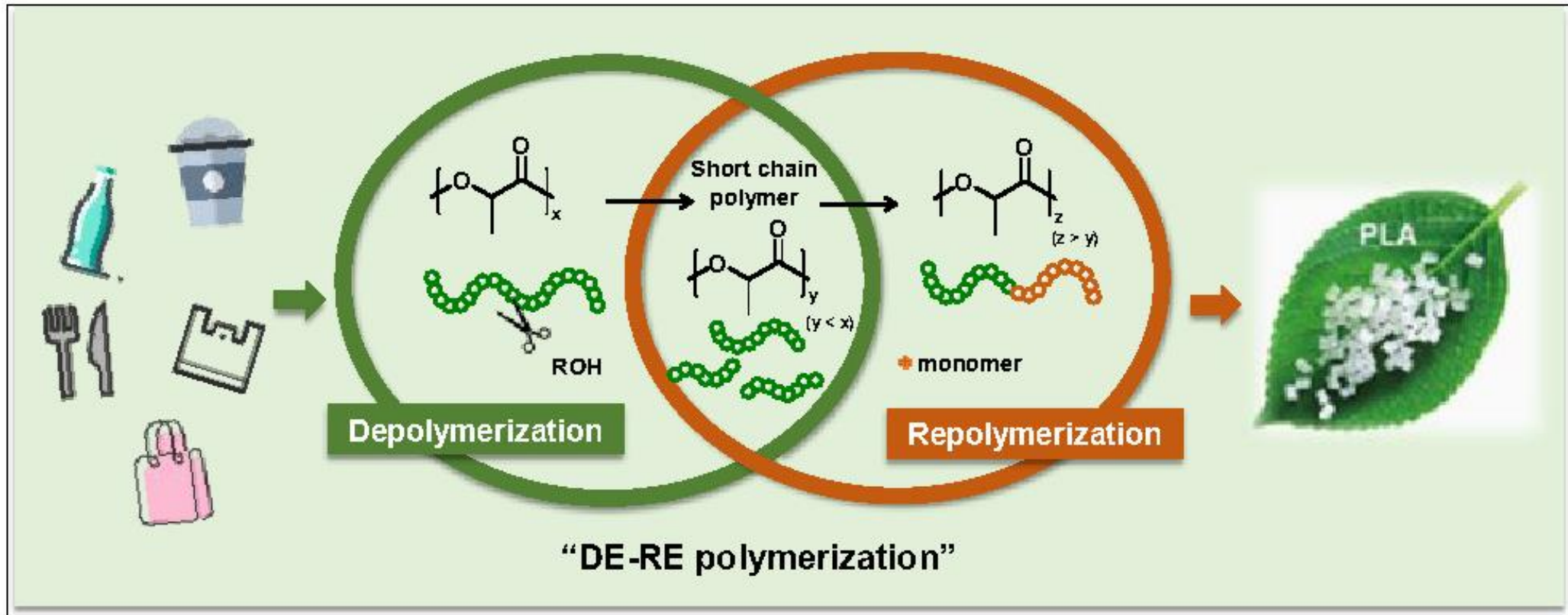


Chemical Recycling

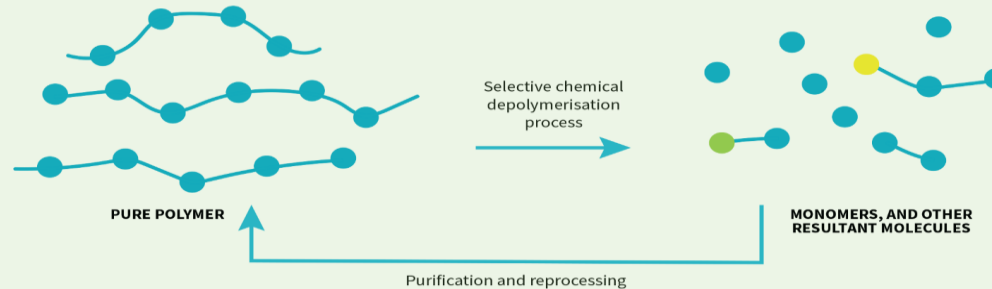


Chemical recycling

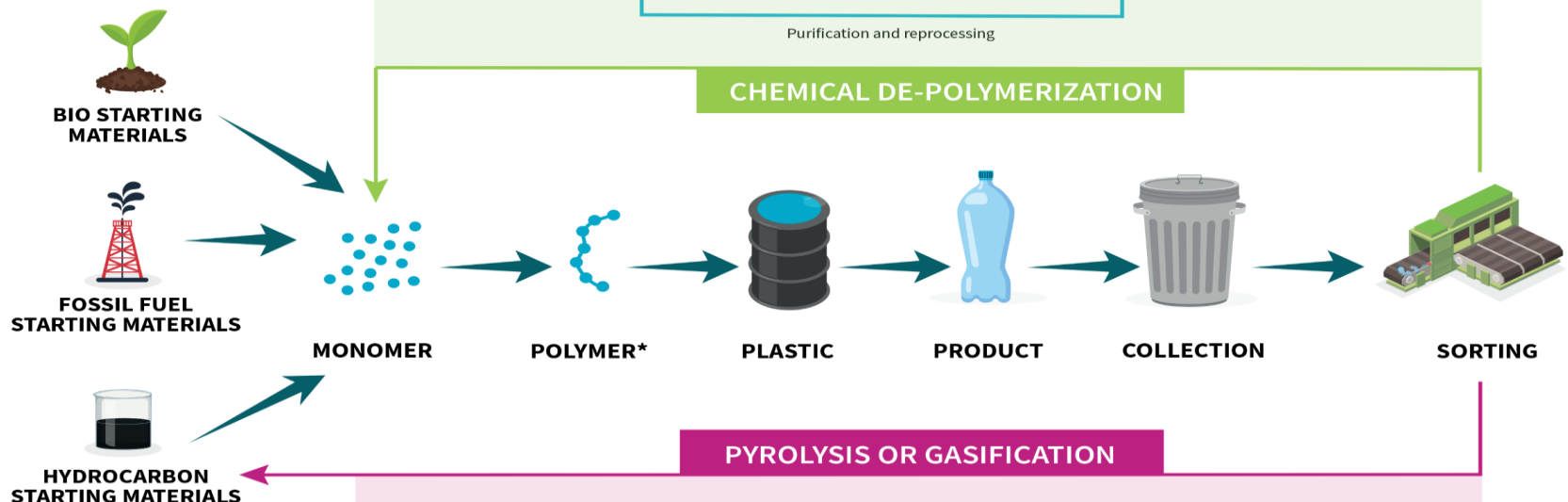
turning plastic waste back into base chemicals and chemical feedstocks



For chemical recycling to be valuable it either has to be highly selective with the circular economy loop really small – taking a pure feedstock and selectively turning it back into the same monomers to reform identical polymers...

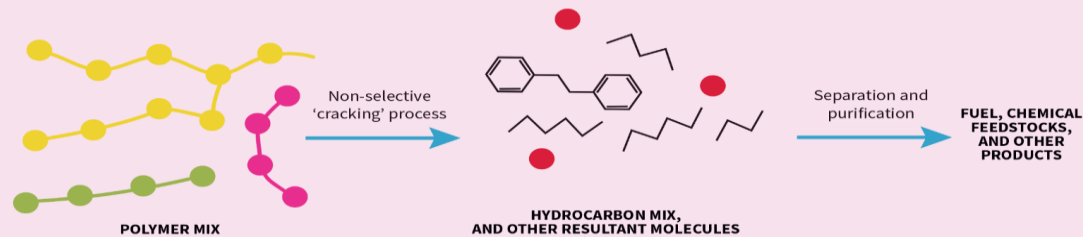


CHEMICAL DE-POLYMERIZATION

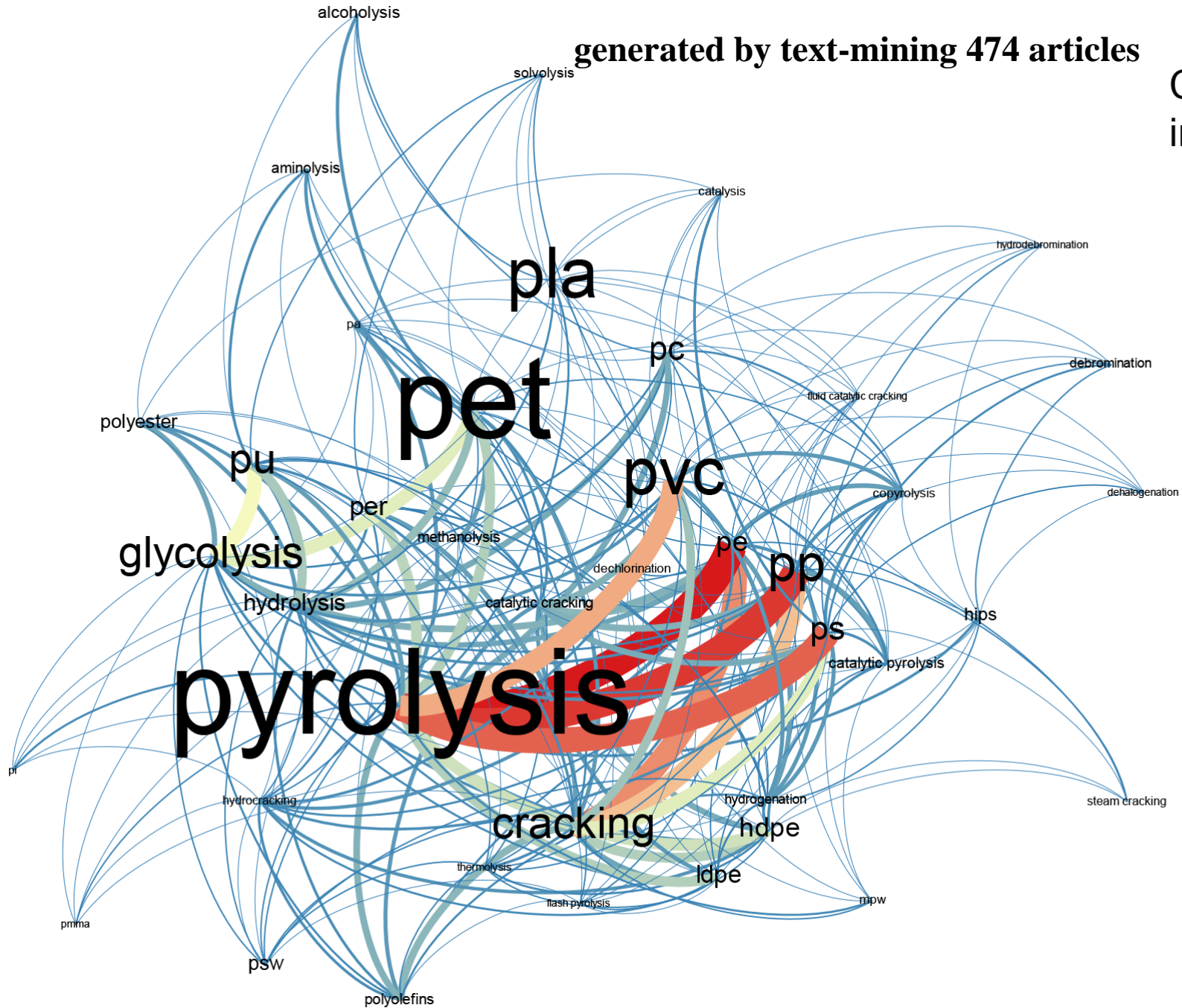


PYROLYSIS OR GASIFICATION

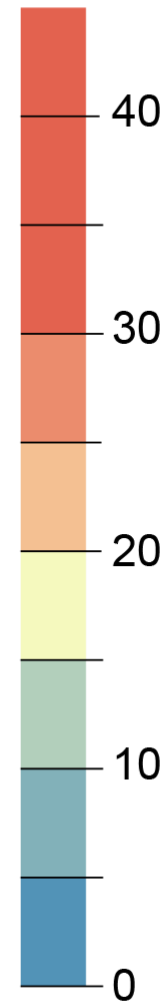
...or have a broad intake of types of plastic, and use a non-selective thermal process to make a mixed hydrocarbon product, which can be fed into existing infrastructure



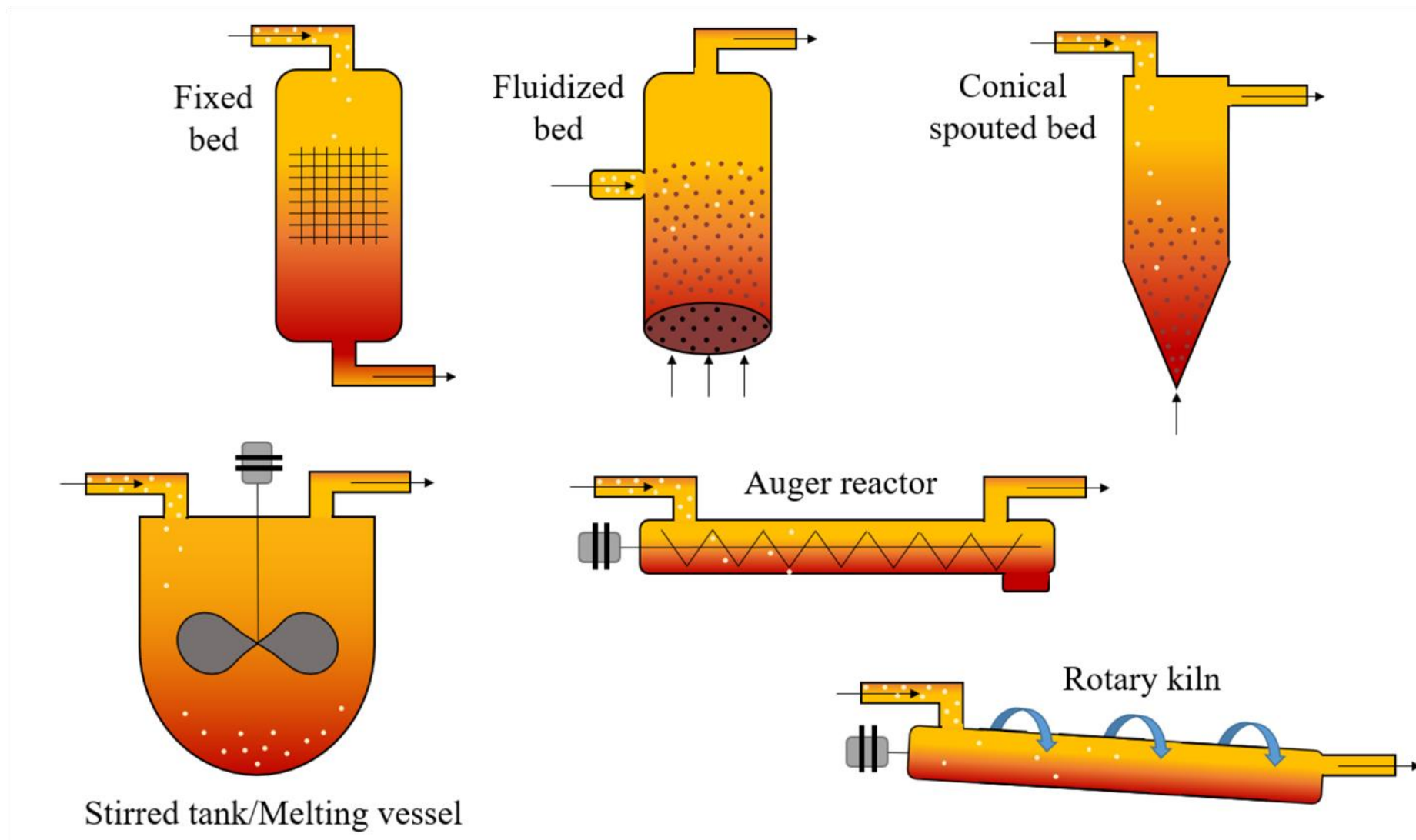
generated by text-mining 474 articles



Co-occurrence
in one paper:

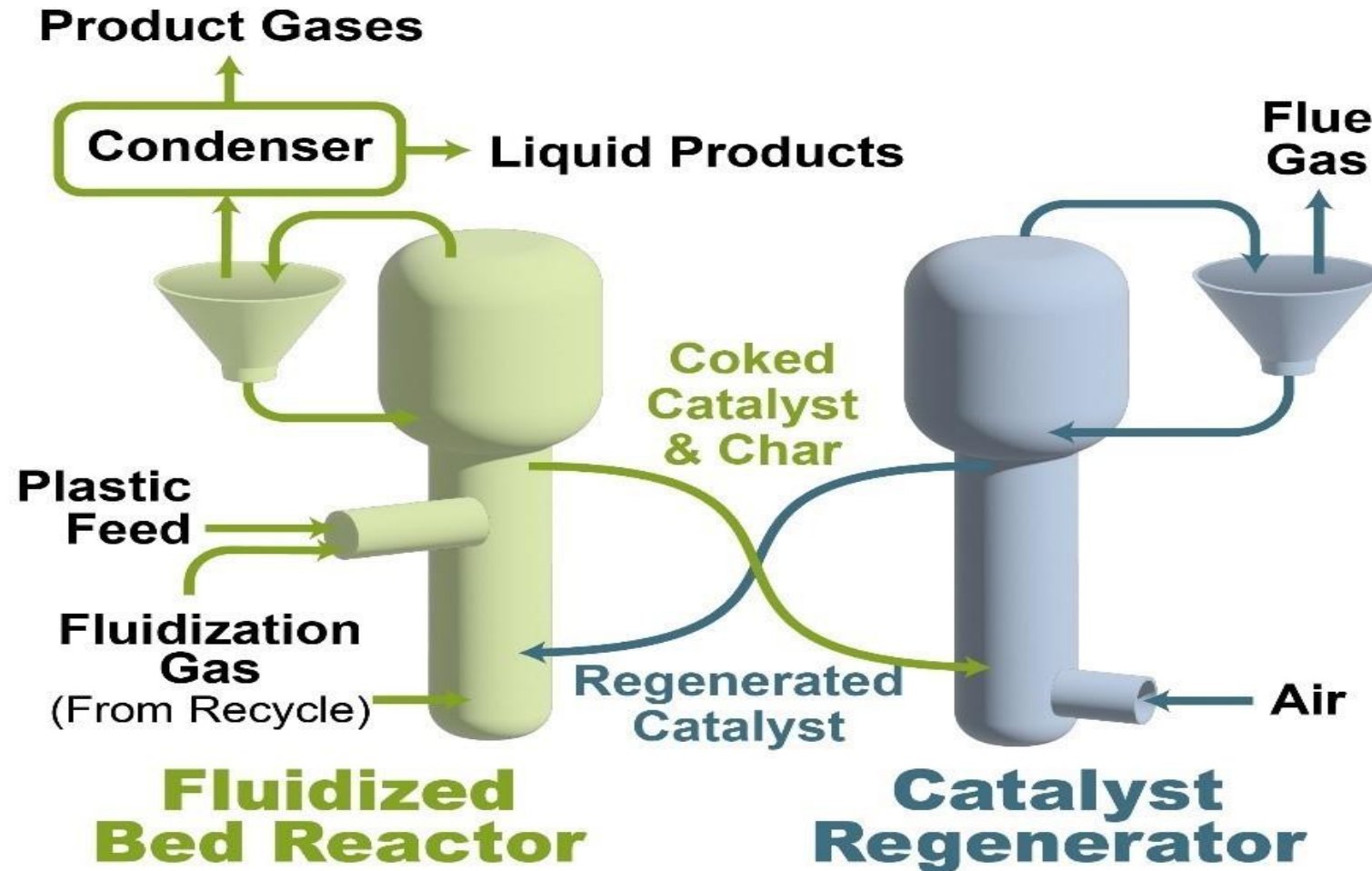


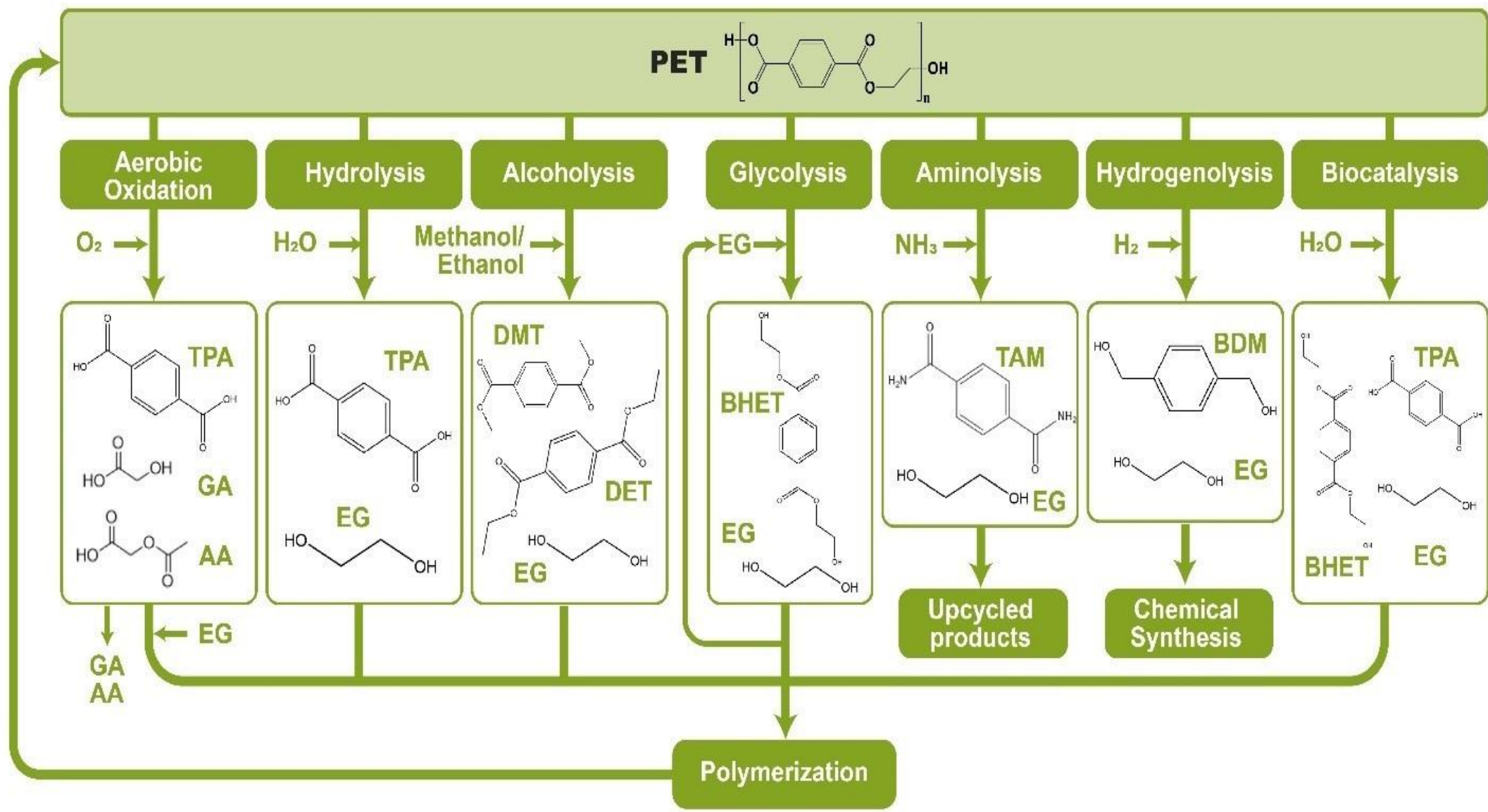
keyword	occurrence
pyrolysis	2267
pet	2156
pla	1236
pvc	1166
pp	879
glycolysis	705
pu	662
pc	500
ps	498
pe	380
hydrolysis	279
aminolysis	108
polyolefins	107
methanolysis	83
solvolysis	70
catalysis	47
pa	44



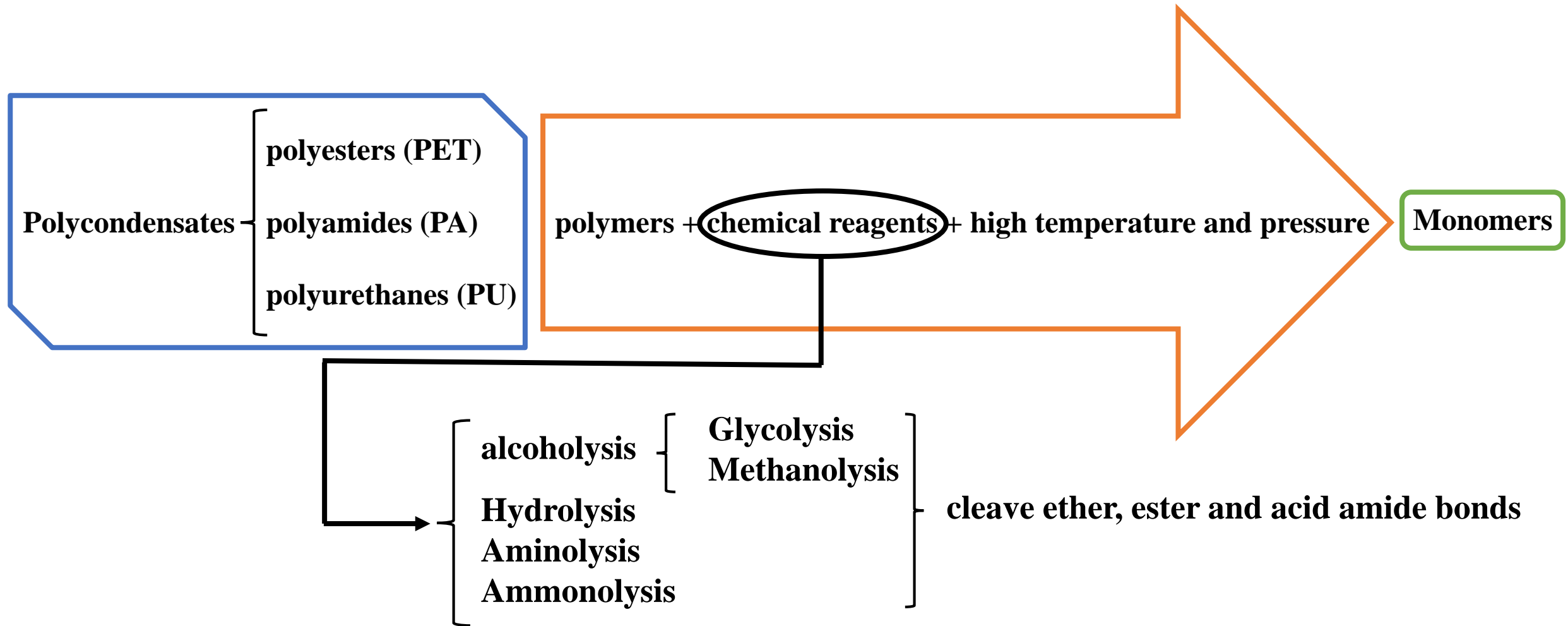
Process	Usual input	Usual output	Benefits	Limitations
Solvolysis	Polycondensates	Monomers and oligomers	Produces monomers and oligomers, which can then be reformed into polymers	<ul style="list-style-type: none"> - Cannot be used to break carbon-carbon bonds, so only works on polymers with specific groups in their chain - Often requires a very pure waste stream
Pyrolysis	Polyolefins, Polystyrene (PS) and mixed plastics	Hydrocarbon products including gases, oils, and waxes	Can be useful for mixed streams, or where different polymers cannot be separated, eg for multilayer film	<ul style="list-style-type: none"> - Poor selectivity in product, requiring further purification and processing before use as feedstock - Uses high temperatures, and therefore a lot of energy especially in the absence of catalysts
Gasification	All plastics	Synthesis gas ('syngas') made up of CO and H ₂ mainly	Can take mixed waste, but can require pre-treatment	<ul style="list-style-type: none"> - Requires further processing from syngas to hydrocarbons and then to monomers or polymers - Need large infrastructures to be profitable, generally on larger scale than pyrolysis plants - Very high energy due to temperatures needed
purification	Polyolefins, Polystyrene (PS), PVC and others	Pure recycled polymers	<ul style="list-style-type: none"> - Useful when there is a known additive to be removed before reformulation - Produces a high purity recycled polymer - Theoretically a step-by-step solvent process could deal with a mixed polymer stream 	<ul style="list-style-type: none"> - Potentially high environmental impact depending on type of solvents used - Polymer can be degraded during process as with mechanical recycling

Fluidized bed reactor for plastic pyrolysis





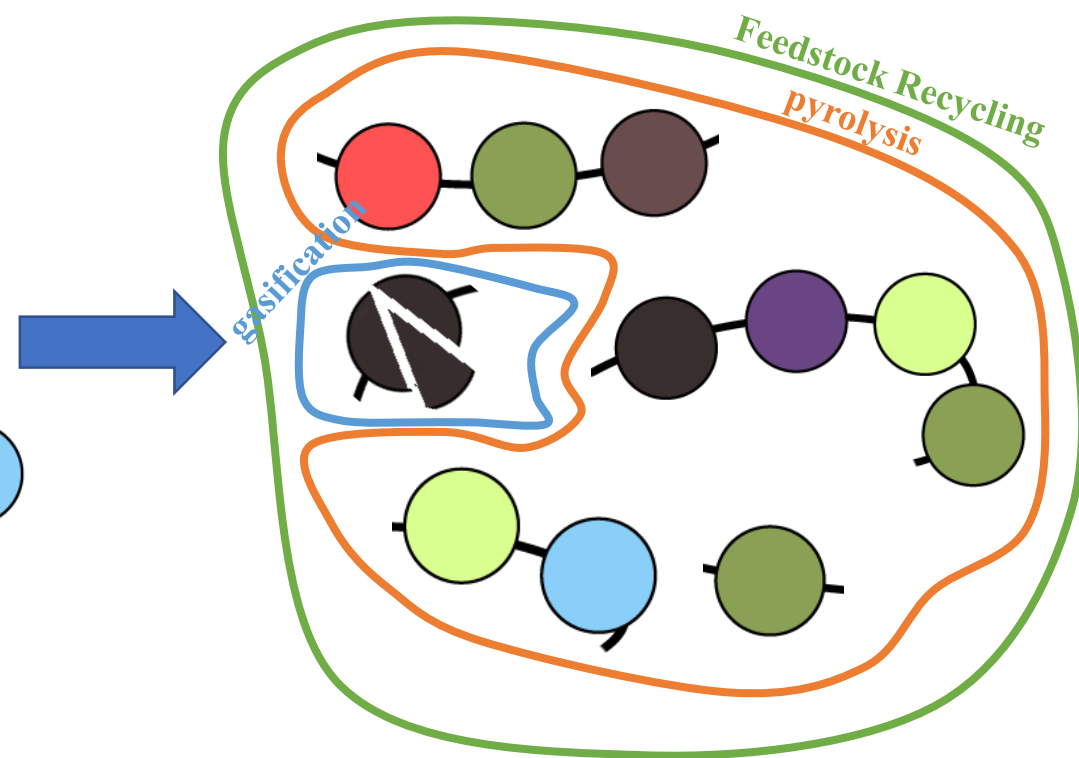
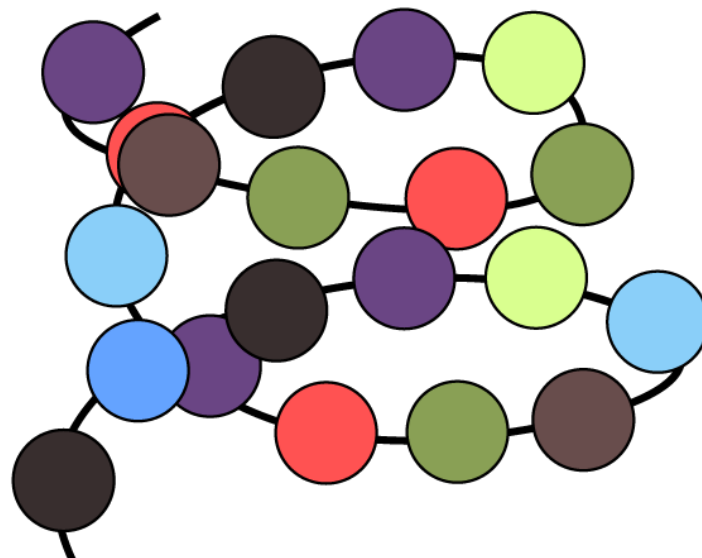
Depolymerization (Chemo lysis / solvolysis)



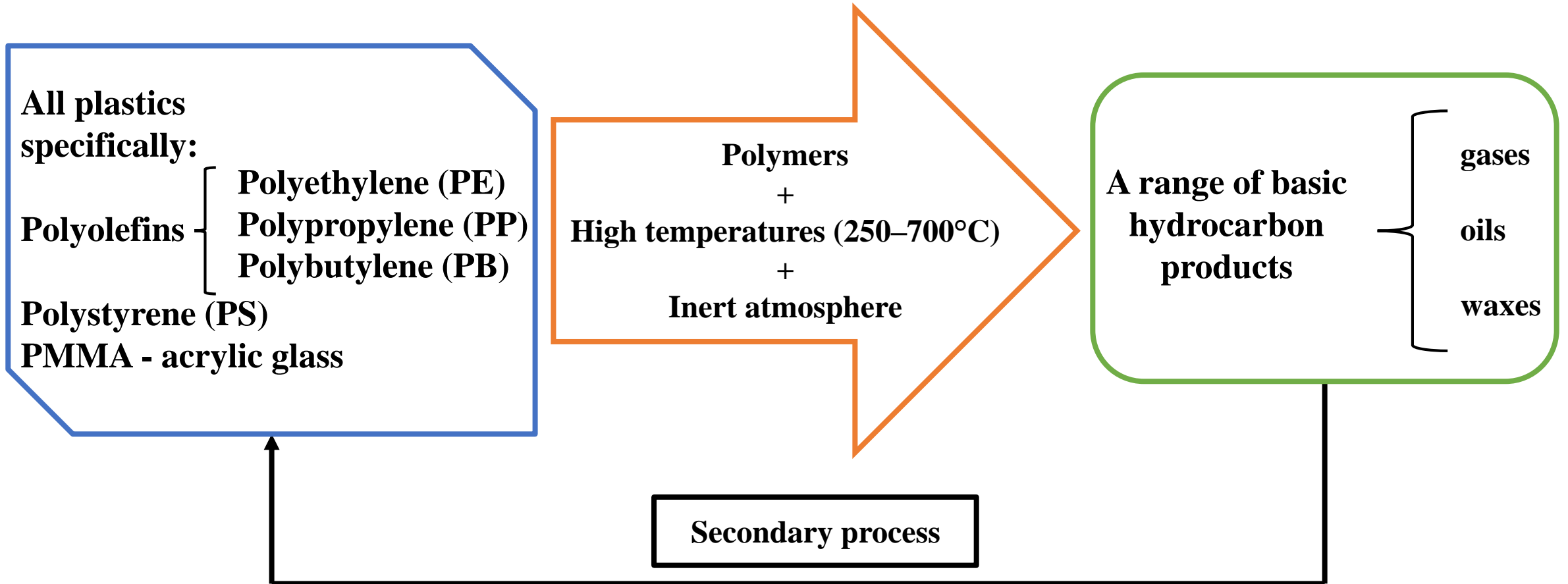
Feedstock Recycling



The two main processes:
pyrolysis
gasification

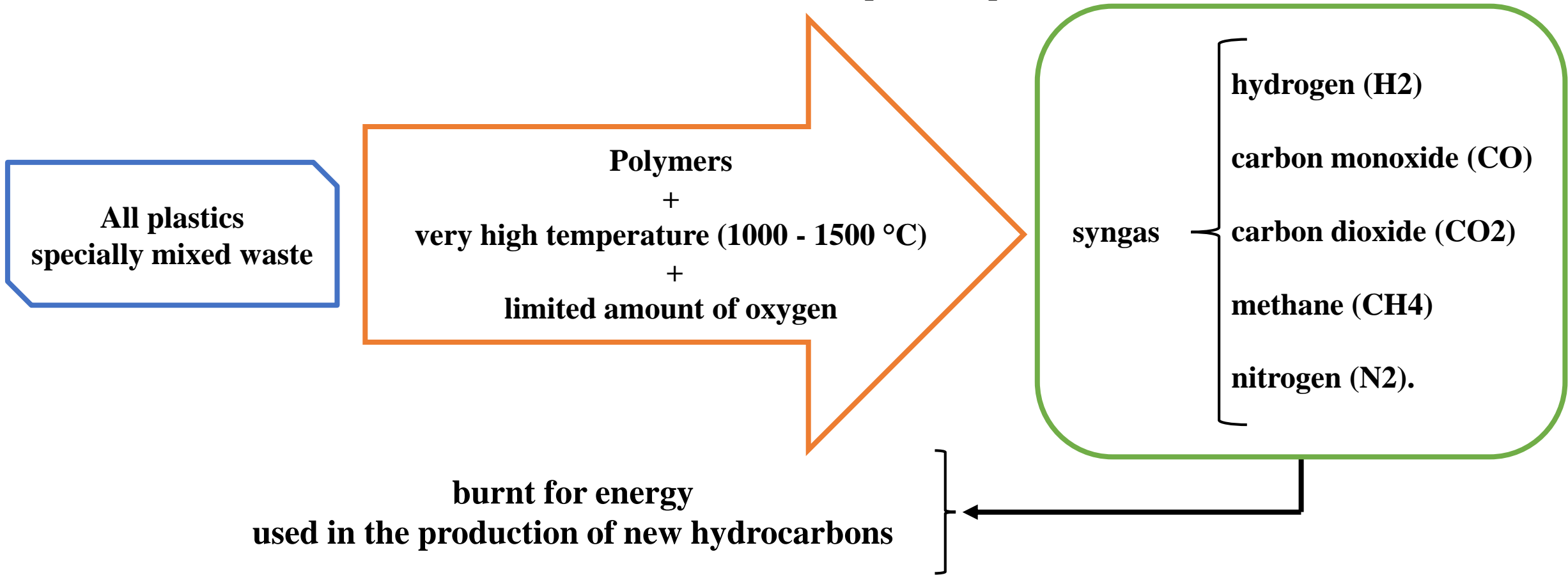


Pyrolysis



Gasification

breaks the molecules down to their simplest components



Summary of waste plastic techno-economic analysis pyrolysis articles by feedstock, products, region, capacity, capital cost, and return on investment (ROI).

Technology	Feedstock	Major Products	Region	Capacity (kton/year)	Capital Cost (MM USD)	NPV (\$) Net present value
Pyrolysis	PS, PP, PE	Heavy oils Petrochemical feedstock	United Kingdom	0.7 – 701	1.36 – 77.2	0.44 /kg – 0.71 /kg
Pyrolysis + upgrading	PS, PP, PE, PET	Hydrocarbon Fuel	Korea	260	\$ 118MM	0.062 /gal
Pyrolysis	PE, PP, PET	Diesel Power Char	Australia	14.6	3.76 MM	2.03 MM
Pyrolysis & Heat Integration	HDPE	Ethylene Propylene	United States	193	118.5MM - 120.5 MM	\$367.8MM - \$383MM
Fast Pyrolysis (Open-loop & closedloop)	Mixed Polyolefins mainly LDPE and residual PP	Naphtha	Belgium	120	Not disclosed	open loop: 32.5/ton Closed loop: 2.72 /ton
Pyrolysis	Plastic waste (PP, PE, PS)	Light oil Heavy oil	Malaysia	120	58.6 MM	20.9 MM

Literature reporting liquefaction of typical waste plastics

Type of Plastics	Temp. (°C)	Pressure (MPa)	Time (h)	Concentration	Solvent/Gas/Catalyst (%)	Products	Oil Yield (wt%)	Year
				Liquefaction under pressurized gases				
PE, PP, PS (continuous reactor)	400	-	-	-	w/ or w/o ZSM-5	Majority aromatics, some aliphatic liquids and gases	85% (PE, PP); 90% (PS)	1992
MDPE, HDPE, PP, PET or mix	420-450	5	1	66% plastics in Tetralin/waste oil	H ₂ ; w/ or w/o 1 wt% HZSM-5/Ferrihydrite catalyst	Hydrocarbon oil and gases	<u>w/o to with catalyst</u> : 11 to 96% (HDPE); 83 to 98% (PP); 33 to 93% (MDPE)	1994
Mix of HDPE, LDPE, PET and PS	400-440	5.6	0.5-2	50% plastics in Tetralin, decalin, dodecane, C ₁₂ -C ₂₀ alkanes	H ₂ ; 10-20 wt% HZSM-5/FCC catalysts	Hydrocarbon oil and gases	56.2-75.8% conversion (mixture); 90-100% conversion (individual plastics)	1996
PS and SBR	350-450	3.45-17.23	0.25-2	1-5 wt% Fe ₂ O ₃ /SO ₄ ²⁻ and ZrO ₂ /SO ₄ ²⁻		Aromatics (PS); Aromatics and C ₅ -C ₉ paraffins/cycloparaffins.	80.3% (PS); 72% (SBR)	1996
LDPE, PET, PVC	420-440	5.5	0.25-0.3	70% in Tetralin	Hydrogen	C ₉ -C ₄₀ hydrocarbons and gases	59% (LDPE)	1996
MDPE, HDPE, PP	> 420	0.68-5.5		30-50% in Tetralin; H ₂ or N ₂ ; HZSM-5 or Al ₂ O ₃ -SiO ₂ -ferrihydrite		Light, medium and heavy oils	> 90% (all plastics)	1996
HDPE, PP, PB	350-450	3.5-13.8	0.5-3	n-octadecane; H ₂ ; 1-2 wt% Fe ₂ O ₃ /SO ₄ ²⁻ and ZrO ₂ /SO ₄ ²⁻		Gasoline range paraffins as major products	> 90%	1997
PE and PP	500	0.79	0.5	Hydrogen		Light and heavy oils	up to 60%	1998
Post-consumer plastic (PCW) mixture	415-455	1.4	0.5-1	H ₂ , 1-5 wt% of HZSM-5 and others		Higher gasoline range oil with catalysts	up to 85%	1999
PE, PP, PS, PVC, and PET (standalone and mixed)	500	1	1	Nitrogen and Hydrogen		Hydrocarbon oil and gases with high concentrations of alkanes and single-ring aromatics	<u>Calculated mix vs. PCW (DSD/Waste Fost Plus)</u> : 72.3% vs 32.5/64.1% (N ₂); 75.12% vs 48.2/70.6% (H ₂)	2007

Type of Plastics	Temp. (°C)	Pressure (MPa)	Time (h)	Concentration	Solvent/Gas/Catalyst	Products (%)	Oil Yield (wt%)	Year
					Hydrothermal Liquefaction			
PVC	200-600	1.6-55.7	1	0.1-2	None	Low-molecular weight aromatic and aliphatic compounds	179ppm (300°C), 396ppm (400°C)	2004
Model mix of PE, PP, PS and PVC	200-400	1-5		100-200	glass powder additive	Chlorine content after NaOH-based dechlorination	40-120 ppm in oil (negl.)	2011
PBT, PC, PLA, PMMA, POM, PPO, PVA, SB.	400	25	0.25	10	None	Oil%/solid%: nil/50.8 (PBT), 99.8/nil (PC), /68.5 (PET), 48/nil (PMMA), 13.7/8.1 (POM), 78.9/8.8 (PPO), 35.4/2.9 (PVA), 80.8/1.2 (SB)		2017
High Impact PS (HIPS)	350-550	30	0.12-1	1-9	None	Ethylbenzene (51.3wt%), Toluene (14wt%) and other polyaromatics (490°C/1 h)	Maximum carbon Liquefaction rate of 77wt% (490°C, 1 h)	2019
PP	425-450	23	0.5-4	-	None	80% naphtha	91% (2 h/425 °C; 1 h/450 °C)	2019
ABS, PA6, PA66, PET, Epoxy, PC, PUR, HDPE, PVC, LDPE, PP, PS	350	corresp. to T	0.33	5.6	KOH	Bisphenol-A & phenol (PC, Epoxy), caprolactam + (PA6, PA66), TE & EG (PET), TDA + (PUR) and no polyolefnderived products		2020
PP, PS, PC and PET	350-450	25+	0.5-1	0.06-0.35	None	32% (PP, 425°C, 30 min), 16% (PET, 450°C, 30 min), 86% (PS, 350°C, 30 min), and 60% (PC, 425°C, 30 min).		2020
PC	350-450	corresp. to T	0.03-0.5	5	None	IPP, IPrP, phenol, BPA, and other alkylphenols	57.7	2020
HDPE	400-450	corresp. to T		57.1	None	Naphtha, heavy oil and heavy waxes	86-87% (425°C, 2.5 h or 450°C, 0.75 h)	2020
LDPE, HDPE	380-450	corresp. to T	0.25-4	20	1% acetic acid	Alkanes, alkenes, cycloalkanes, aromatics, and negligible alcohols	85-90% (425-450°C, 1 h)	2020

Example of a continuous tubular reactor design for hydrothermal liquefaction of plastics
(Extracted from the US patent US 8,980,143 B2).

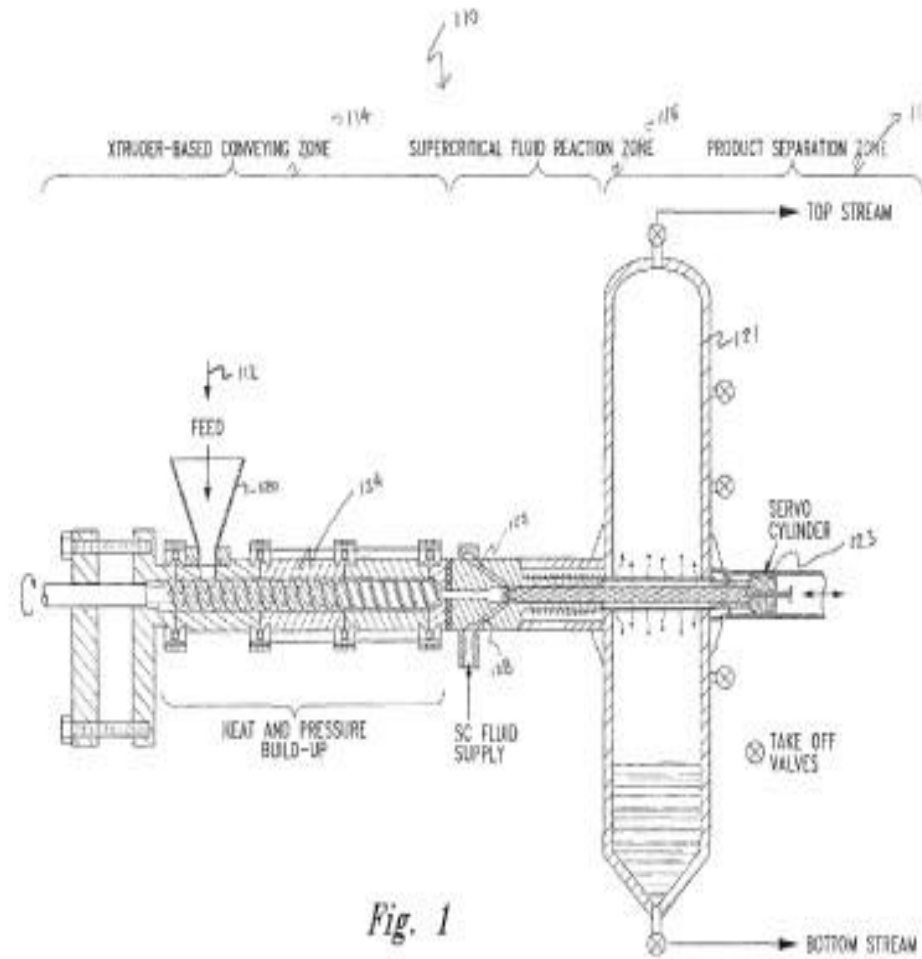
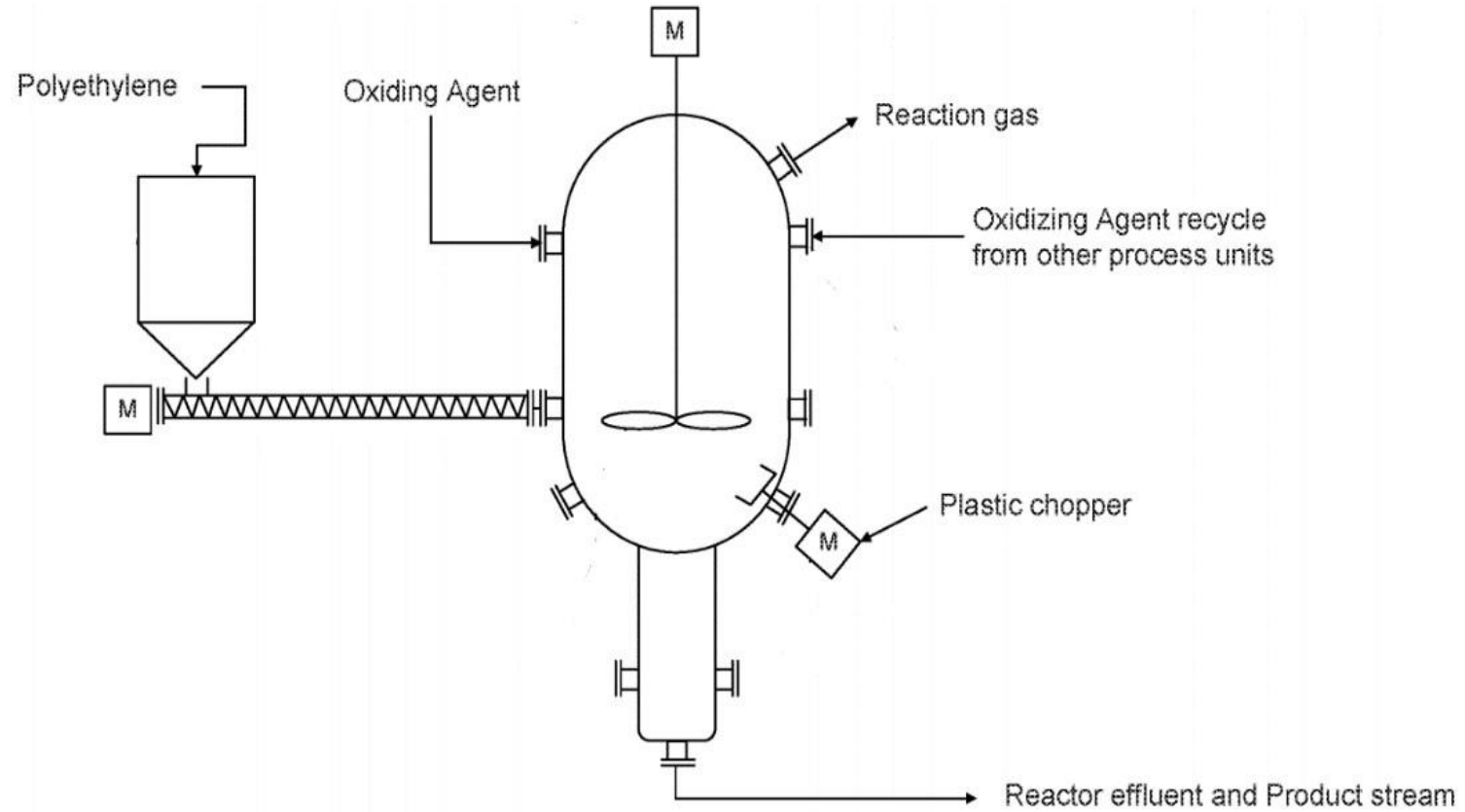


Fig. 1

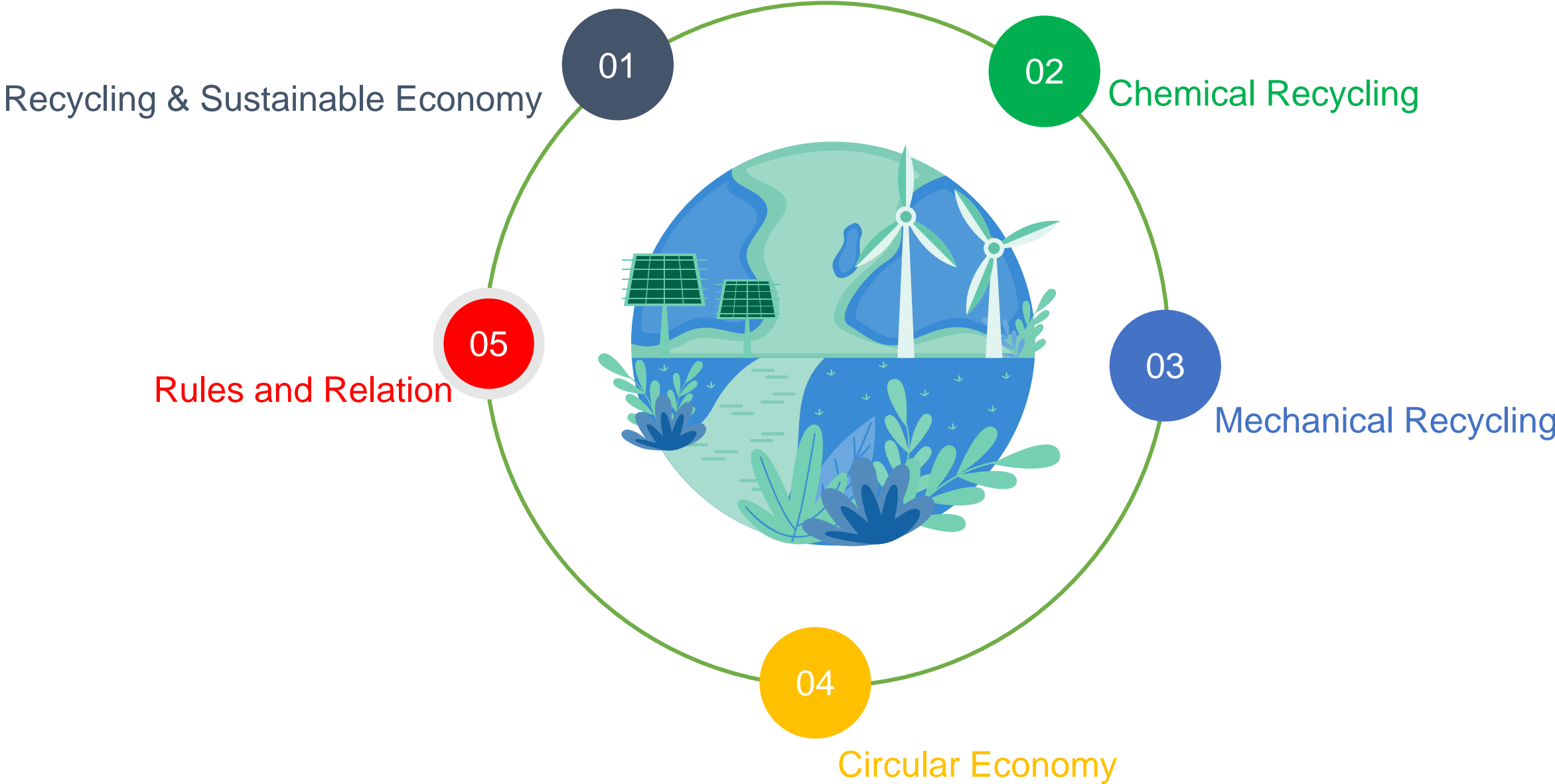
Hydrogenolysis of Plastics into Various Hydrocarbons in Batch Reactors.

Catalyst	Polymer	Temperature (°C)	Pressure (Bar)	Time(h)	Polymer/Catalyst (Mass)	Products
Ru/CeO ₂	LDPE, HDPE, PP	200-240	20-60	5-24	34	Liquid fuels, waxes (C5-C45)
Ru/TiO ₂	PP	250	30	8-16	20-40	Lubricants (C20-C60), C1-C2 gases
Ru/Nb ₂ O ₅	PET, PS, PC	200-320	3-5	12-16	1-2	Aromatic hydrocarbons
5Ru/C	PE, LDPE	200-225	20	16	25	Liquid alkanes (C3-C13), light gases (C1-C6)
5Ru/C	PP	250	35	8-24	14	Liquid alkanes (C5-C32), light gases(C1-C5)
Ru/FAU	LDPE, PP	300-350	50	3	50	Methane, light paraffins (C2-C11)
Ru/WO ₃ /ZrO ₂	LDPE	250	30	2	40	Lubricants, waxes, diesel (C4-C35)
Ru/C	HDPE	220	30	1	2	Lubricants, liquid fuels (C6-C38)
Pt/WO ₃ /ZrO ₂ +Zeolite	LDPE	250	30	2	10	Liquid fuels (C5-C22)
Pt/SrTiO ₃	PE	300	12	96	5	Lubricants, waxes (Mw 2001000 Da)
SiO ₂ /Pt/SiO ₂	HDPE	300	14	24	88	Fuels, lubricants (C8-C32)
Pt/C	PP	300	15	24	10	Lubricants (C5-C45)

Strategies in functionalization of plastics: (A) Functionalization of polyolefins; (B) oxidation of polyisobutene; (C) PLA amination; (D) reactive extrusion



Conclusion



A close-up photograph of a vibrant red rose, its petals glistening with numerous small water droplets. The rose is positioned diagonally across the frame, with its green stem and a few leaves extending towards the bottom left. The background is a dark, textured grey, which makes the bright red of the rose stand out prominently. The lighting is soft, highlighting the texture of the petals and the individual droplets.

Thanks for your Attention